

## **USER MANUAL**

# LABORATORY BIOREACTORS 15.1 & 15.2



User Manual Ref: BioReactor15\_rev 1.1

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### 1. INTRODUCTION

The following user manual enables safe and efficient handling of the further listed equipment. It contains instructions which describe the installation, operation and maintenance procedures of the laboratory bioreactor system 15.1 & 15.2, operation of the bioprocess controller and the SCADA (supervisory control and data acquisition) software. The user manual is an important part of the bioreactor equipment and should be kept accessible to the system operators at any time.

Before starting any work with the bioreactor system and its components, it is strongly recommended to carefully read this user manual. Full understanding of the described procedures in this document is of utmost importance for user, equipment, and process safety. Only competent and trained personnel should perform operation and maintenance procedures of the bioreactor system.

In case if additional customer service or information is required, please contact your local supplier Froilabo at +33 (0) 4 78 04 75 75 or e-mail us at commercial@froilabo.com

### 2. DESCRIPTION OF THE EQUIPMENT

The bioreactor system consists of two functional parts:

Autoclavable vessel, equipped with an upper lid and inputs/outputs (ports), agitator axle with a magnetic drive, impeller turbines, baffles, gas sparger;

Bioprocess controller is equipped with a peristaltic pump system, power control unit, gas supply system, and a thermostat.

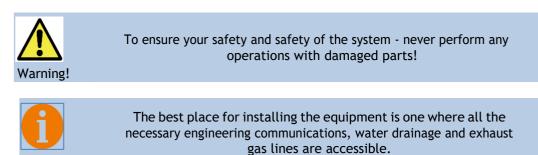
The bioprocess controller ensures:

- Temperature (the temperature sensor (Pt100) is located in the bioreactor tank) regulation. Carried out by supplying a control signal either to the heating element or the electro-magnetic cooling water valve of the thermostat. Thermoregulation is carried out by circulation of thermostated water through the bioreactor's jacket, which is located in the bottom lid of the vessel;
- 2) pH control. Carried out by supplying base or acid solutions to the bioreactors medium using the bioprocess controller's peristaltic pumps;
- 3)  $pO_2$  control. Ensured by automatic adjustments of the stirrer's rotational speed. The actual  $pO_2$  value is monitored using a  $pO_2$  electrode;
- Foam control. Carried out by supplying an antifoam agent to the bioreactor's medium using the bioprocess controller's peristaltic pumps. The foam level is monitored using a conductivity sensor;
- 5) Feeding (of a substrate). Carried out using the bioprocess controller's peristaltic pump and the respective feeding rate/volume is controlled by the feeding profile, which is set in the bioprocess controller;
- 6) Level control. Carried out using the bioprocess controller's peristaltic pump. The medium level is monitored using a conductivity sensor;
- 7) Mixing. Ensured by a magnetic drive (stirrer inner shaft and impellers contain magnets), the agitator is driven by a motor which is mounted on the top lid of the bioreactor.

### 3. EQUIPMENT INSTALLATION AND ASSEMBLY

After receiving the equipment, we strongly recommend carrying out a visual inspection of the system. Inform the installation engineer or Froilabo about any visible damage of the equipment.

- 1) Install the bioreactor in a dry, free from dust and any other potential contaminants location;
- 2) The system should be installed away from any intense sources of heat. The appropriate temperature of operation for the bioprocess controller is between 5 °C and 42 °C;
- 3) Ensure a minimal space of between 15 20 cm at the back and on the sides of the bioprocess controller to eliminate any difficulties while installing, working and maintaining the equipment.



#### 3.1 INSTALLATION OF THE BIOREACTOR VESSEL

To ensure correct system functionality, each of its components must be installed in line with the instructions described further.



Notice!

Failure to comply with the instructions may cause failure in the operation of the equipment and may result in permanent damage!

As was stated earlier the bioreactor consists of the following two basic parts: (1) an equipped bioreactor vessel (2) and the bioprocess controller (see Figure 3.1).

### 3. EQUIPMENT INSTALLATION AND ASSEMBLY



Figure 3.1. Bioreactor system schematic

While installing the bioreactor, the vessel should be placed on the left side of the control unit as shown in Figure 3.1.

If it is necessary, and in order to make the reactors assembly more compact (so that it can be conveniently placed in an autoclave, etc.), the option of lowering the output air condenser has been provided (see Figure 3.2). To raise or lower the output air condenser, start by pressing the button indicated by the PUSH arrow 1 (see Figure 3.2 - A, B). Without releasing the button, lower (see Figure 3.2 - A, LOWER) or rise (see Figure 3.2 - B, RAISE) the output air condenser. Release the button only after achieving the desired position of the condenser.

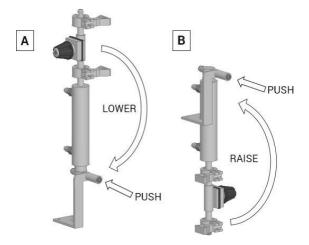


Figure 3.2. Raised (A) and lowered (B) output air condenser, with arrow indicators for raising or lowering it

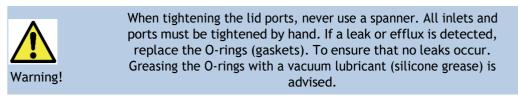
After installing the bioreactors tank and the control unit, connect the respective inputs and sensors as shown in Figure 3.8.

#### 3.2 DESCRIPTION OF THE REACTOR LID AND PORTS

As a part of a standard set-up, the reactor's lid (see Figure 3.4) contains twelve ports for the following:

- Sensor connections (five ports);
- Bioreactor's liquid supply (three ports);
- Gas sparger and gas output port (two ports);
- Two spare ports that can be used according to the users preferences.

For the bioreactor's liquid supply (see Figure 3.4), the use of septa, one or three-way inlets has been envisioned (see Figure 3.3 - A and B, respectively). The standard set includes three ports with a one-way inlet, one port with a three-way inlet and a septa port for inoculum injection.



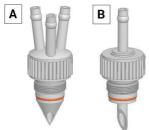
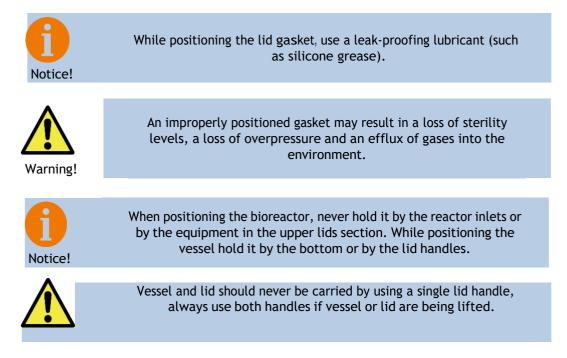


Figure 3.3. Ports with a one-way (A) and a three-way (B) inlet

The mounting procedure of the bioreactor lid on the vessel is done as follows:

Place the GASKET between the bioreactor's upper lid and the vessel in the cavity seen in Figure 3.4. The lid is placed on the reactor tank by holding it by its handles.



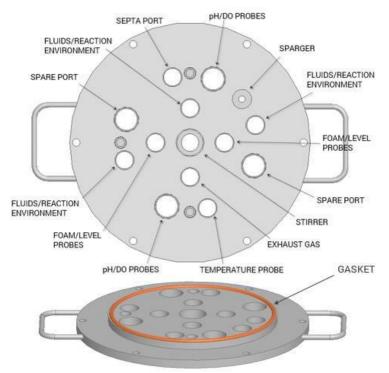
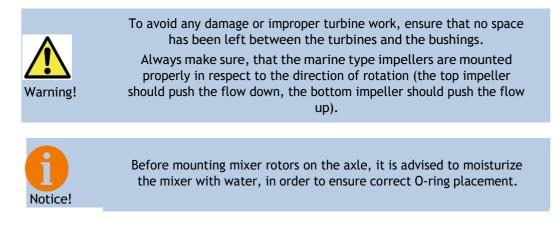


Figure 3.4. Chart showing the upper lid ports and gasket

While cleaning the bioreactors vessel, the occasional removal and cleaning of the stirrer impellers is recommended. In order to carry out this procedure, please follow the instructions described below (see Figure 3.5).

To remove the turbines, first loosen the screw on the upper lid that holds the sparger in place and then turn the bioreactors sparger from its initial position (see Figure 3.5 - A) to the position shown in Figure 3.5 - B. Remove the circlip with provided pliers and proceed by pulling one turbine at a time in the direction that is opposite to the bioreactors lid, take off each turbine and silicon carbide bushing individually from the stirrers' axle (see Figure 3.6 - B).

The silicon carbide bushings, circlips and turbines should be placed back in the same order in which they were removed (Figure 3.6 - A, B). The order for placing the impellers back is of particular importance due to their different dimensions and paddle orientation. The silicon carbide bushings may be swapped places without causing any problems.



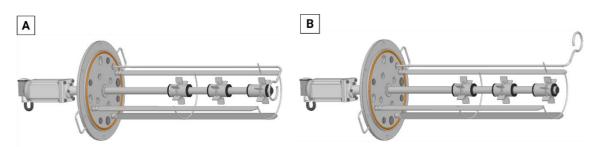


Figure 3.5. Two sparger positions. A - the operating position of the sparger; B - the sparger in its turned position thus allowing the removal of the turbines



Figure 3.6. Removal of the reactor turbines. A - disassembled turbines and turbine bushings; B - correctly assembled stirrer paddle-type turbines if the turbines rotates counter-clockwise (looking from top of the lid) (for Rushton type turbines turbine rotation direction do not influence mixing quality!).

Correct positioning of the stirrer impellers is of utmost importance in order to ensure their proper work. The turbines should be placed opposite the stirrers inner axle magnets. The position is chosen according to the magnetic force principle. This procedure is carried out by moving the impeller along the bioreactors axle until the magnetic power fixes the rotor to the correct position. After the proper position of the impellers has been found, the silicon carbide bushings should be moved closely towards the turbines from its opposite ends. It is important to maintain the impeller at its correct position while the bushings are being pushed towards the rotors. Circlips are to be mounted in direct contact with carbide (black) bushing to prevent the bushing from accidental loosening during the process.



To avoid any damage or improper operation of the stirrer, always make sure that the impellers and silicon carbide bushings are placed correctly and in line with the above-mentioned instructions.



After assembling the stirrer it is recommended to perform a test to make sure that the stirrer is assembled correctly: when assembled, rotate the inner axle by hand, if this can be achieved without applying significant amount of force, then the stirrer is assembled correctly.

#### 3.3 SENSOR INSTALLATION

To correctly and safely install sensors into the bioreactor, please follow the instructions described below.

A bioreactor sensor system contains five sensors:

Temperature -		Pt100 temperature sensor;
pН	-	Glass pH electrode;
pO <sub>2</sub>	-	Polarographic pO <sub>2</sub> electrode;
Foam	-	Conductivity sensor;
Level	-	Conductivity sensor.

The installation of pH and pO<sub>2</sub> sensors requires the use of port adapters as shown in Figure 3.7.

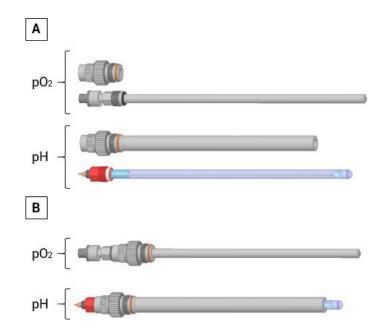
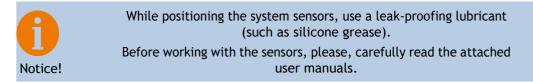


Figure 3.7. pH and pO<sub>2</sub> sensors with port adapters in a disassembled (A) and an assembled (B) state



Insert the pH and  $poi_2$  sensors into the corresponding ports on the upper lid of the bioreactor and screw them in place until they are firmly attached.

#### 3.4 SERVICE CONNECTIONS

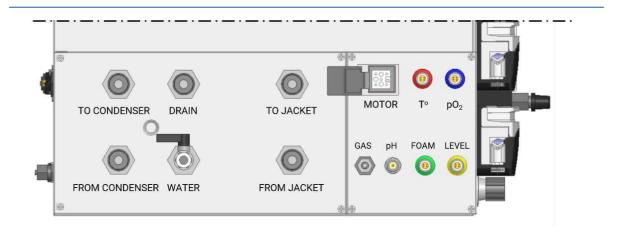
The service connections for the bioreactor system can be found on the left side and in the rear part of the bioprocess controller (see Figure 3.8 and Figure 3.9). Use the supplied hoses and quick connections as shown in Table 3.1.

#### Table 3.1. Service connections

Service	Requirements	Connection type
Air	1.5 bar (Max 2.0 bar!!)	Quick connection
O <sub>2</sub>	1.5 bar (Max 2.0 bar!!)	Compression connection
Water	1.0 - 1.5 bar (Max 2.0 bar!!)	Quick connection
Electrical power	208 - 230V, 50/60 Hz, one phase, 15 Amp (fluctuations do not exceed $\pm$ 10 %)	G series plug
Outlet air	Maximum overpressure 0.5 bar	Quick connection

Descriptions for the designations of Figure 3.8, Figure 3.9 and Figure 3.12 identify all of the service connections for the bioreactor.

- 1) Using the supplied hose, connect the main water input (WATER) to the controller (Figure 3.8);
- Using the supplied hose, connect the water output (DRAIN) to the bioprocess controller (Figure 3.8) and position it into the drainage system;
- 3) Using the supplied hoses, attach the connections TO JACKET / FROM JACKET to the bioprocess controller (Figure 3.8);
- 4) Using the supplied tubes and quick connections, attach the connections TO CONDENSER / FROM CONDENSER to the bioprocess controller (Figure 3.8);
- 5) Using the nylon tube (SMC T0806), attach the AIR connection to the controller (see Figure 3.9);
- 6) Using the nylon tube (SMC T0806), attach the OXYGEN connection to the controller (see Figure 3.9).



#### Figure 3.8. System water service connections (left side of the bioprocess controller)

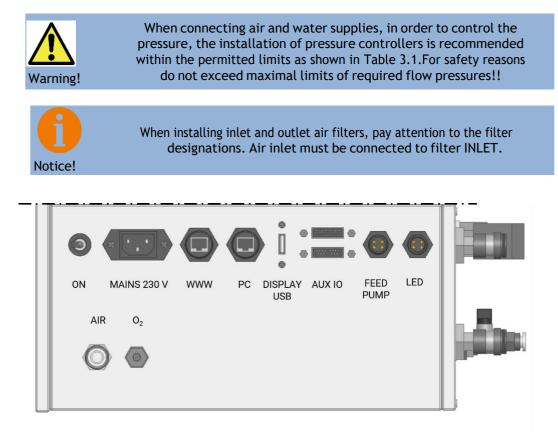


Figure 3.9. Air and oxygen service connections (back of the bioprocess controller)

#### 3.5 VESSEL CONNECTIONS

After carrying out all of the activities listed in Section 3.4: "SERVICE CONNECTIONS", follow the instructions described below:

1) Attach the reactor inlet gas tube with an installed inlet air filter according to Figure 3.10 to the bioprocess controllers GAS outlet (see Figure 3.8). Connect the inlet air tube to the gas sparger port (see Figure 3.4);



Figure 3.10. Inlet/outlet gas pipes and filter set

- 2) Connect the outlet gas tube with its filter (see Figure 3.10) to the outlet air condenser at the location specified in Figure 3.11;
- 3) Connect the quick connections marked TO CONDENSER / FROM CONDENSER (Figure 3.8) to the outlet air condenser as shown in Figure 3.11;

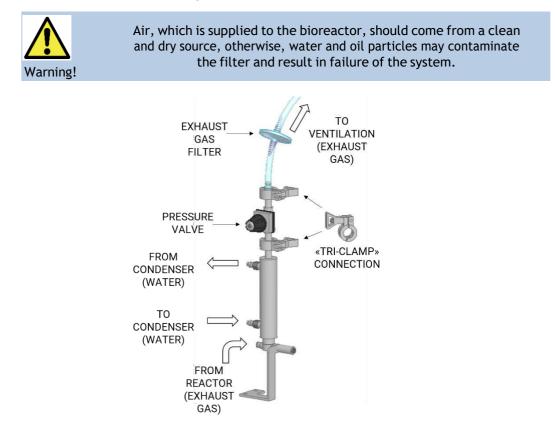


Figure 3.11. Outlet air condenser connections

- 4) Perform the connections TO JACKET/FROM JACKET (Figure 3.8) to the thermostating jacket outputs (see Figure 3.1). It is recommended to connect the TO JACKET tube to the lower thermostating jacket connection, but the FROM JACKET tube to the upper jacket connection;
- 5) Attach T, pH, pO<sub>2</sub>, LEVEL and FOAM cables to the respective sensors. Then connect them to the bioprocess controllers respective ports shown in Figure 3.8;

To install the motor, carry out the steps described below:

- 1) Turn the motor's clutch into an appropriate position, so that the inner axles connection fits inside the motors connection (see Figure 3.12– A);
- 2) Place the motor on the stirrers axle (see Figure 3.12 B);
- To check whether the connections are fitted correctly, perform a visual inspection through the motors window (see Figure 3.12 - C);
- 4) Using minimal force carefully tighten the motor screw (see Figure 3.12 D).

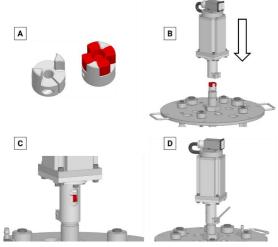
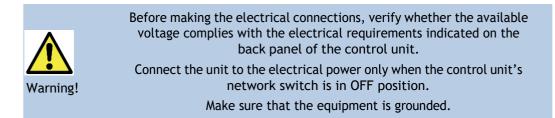


Figure 3.12. Motor installation

To install the peristaltic pump tubing, see Section 10.1: "TUBING".

#### 3.6 POWER CONNECTION

In Section 3.5: "VESSEL CONNECTIONS" electrical power connections for the motor and system sensors were described. In order to start work with the laboratory bioreactor, make the following connections (see Figure 3.9).



Perform the service and device connections on the back side of the bioprocess controller:

- 1) Connect the electrical cable to the POWER 230 V input;
- 2) Connect the internet cable (if required) to the WWW input;
- 3) Connect the computer cable (if required) to the PC input;
- 4) Connect the external feeding pump (if required) to the FEED PUMP input.

It should be noted that the standard biocontroller, includes a built-in internal UPS (uninterruptible power source). In case if any interruptions in the power supply occur, UPS can ensure the operation of the bioprocess controller for up to 15 minutes. Online data storage in the database is ensured within this time interval.

### 4. SPECIFICATIONS

In Table 4.1 the main specifications of the 15 L laboratory bioreactor are listed.

Notwoight	Control unit	30 kg
Net weight	Vessel	30 kg
Overall dimension (mm)		Width 1000, depth 600, height 970 (m)
Controller		15" colour touchscreen
		Flexible software for process control
		Built-in Wi-Fi router for connection with SCADA and other computer software for wireless control
		Built-in UPS power supply source
Electric power	Supply 100 - 240 V	AC
parameters	Power 1000 W	
Materials	Process	All process inputs, valves and related structural elements are made of 316L stainless steel (polished), 100 % boron silicate glass, polyurethane (water inputs), nylon (gas inputs - air, $O_2$ , nitrogen, etc), zirconium oxide and silicon carbide ceramics, plus Teflon
	Non-process	316L or 304 type stainless steel
	Gaskets and O- rings	Rubber
Temperature	Sensor	Platinum Pt100 RTD sensor
	Control performance element	During the process, the temperature in the bioreactor is controlled trough the jacketed bottom surface. Jacketed bottom surface temperature are controlled with by the thermostated water. The control elements are the electric heater and the electric magnetic cooling valve. All thermoregulation elements are placed in a separate unit, which is connected to the water pipe, sewerage and jacket, which covers the bottom of the bioreactor
	Type of control	PID control
	Range	In normal mode the water supply at a temperature of between 16 – 52 $^{\circ}$ C is used as cooling water (with an insulation jacket of up to 70 $^{\circ}$ C).
Agitation	Drive	134 W 24V BLDC motor with electronic control
	Type of control	PID control or manual settings
	Range	40 - 650 rpm
Aeration	Air filter	0.22 µm filter sterilized by autoclaving
	Type of control	Manual and/or automated with electric magnetic valve
	Range	0.1 - 23.0 sL/min (Air); 0.1 - 8.5 sL/min (Oxygen)
Outlet air	Air filter	0.22 µm filter sterilized by autoclaving
Mixing two gases	Type of control	Manual and/or automated with electric magnetic valves
Peristaltic pumps		Four peristaltic pumps with configured functions (installed on the control unit)

Table 4.1. Main specifications of the 15 L laboratory bioreactor

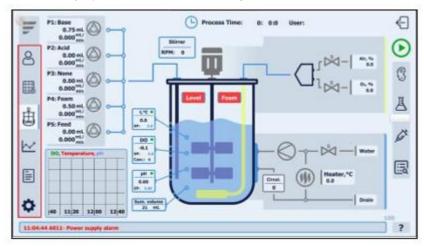
		Option to connect the external feeding pump to an analogue control signal
Foam	Sensors	Conductivity sensor
	Control performance element	Peristaltic pump
Level	Sensor	Conductivity sensor
	Control performance element	Peristaltic pump
pH (facultative)	Sensor	Sterilizable gel pH sensor
	Control performance element	Peristaltic pumps for adding base and/or acid
	Type of control	PID control
	Range	pH 2 - 12
DO (facultative)	Sensor	pO2 polarographic sensor
	Control performance element	$pO_2$ cascade control with stirrer rotation speed, inlet air enrichment with oxygen and feeding speed
	Type of control	PID control
	Range	0 - 150 % from the air content

### 5. BIOPROCESS CONTROLLER

The bioprocess controller ensures control and supervision of the 15 L bioreactor.

The control unit ensures specific parameter set-points (SP) (T, pH,  $pO_2$  etc) can be controlled and actual process values (PV) can be visualized. The operational activity and actual values of some their control actuators (Valves, Pumps, etc) is possible. Extended (*optional*) version of SCADA ensures remote control of most bioreactor's control parameters and actuators.

#### 5.1 DESCRIPTION OF THE INTERFACE



Information about the display/interface is shown in Figure 5.1.

Figure 5.1. Bioreactor control interface

The touchscreen can be activated by touching the screen with a finger or stylus.

#### 5.2 STARTING THE WORK

To start working with the bioprocess controller follow the instructions listed below:

- Turn on the controller by moving the ON/OFF switch at the back of the control unit (see Figure 3.9). The Company logo will appear on the main screen of the bioprocess controller. Touch the screen to proceed;
- 2) The REACTOR window will appear, see Figure 5.2. More detailed information about the functionality of this window is given in Section 5.3: "REACTOR WINDOW";

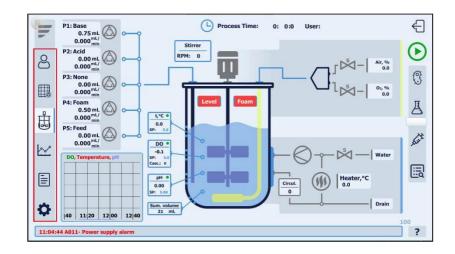


Figure 5.2. REACTOR window



This and all of the following windows can be activated by touching the display with a finger or other object (e.g. a stylus).

3) The MAIN MENUof the bioprocess controller is located on the left-hand side of the user interface (highlighted in 5.2). Press the ADMINISTRATION button, thus opening the ADMINISTRATION window, where the use can log in into the system, see Figure 5.3;



Figure 5.3. Control unit's ADMINISTRATION window

4) Choose the desired access level (Viewer, Operator or Administrator) (Figure 5.4), enter the respective password after clicking on the blank space next to the word password (Figure 5.5), press ENTER and LOGIN.

ji o	t°C:0.0 pH:0.00	DO: -0.1 Case		ents	English   ←
	New user Delete user Change	Date 06/22/20 Password: Successfully le	? •		
<u>k~</u>	password				
<b>¢</b>	Disable alarms			User:	102
	11:04	44 A011- Power supply al	arm		?

Figure 5.4. Access level window

By default, the password for the above mentioned access control levels are pre-set as follows:

User Type	Access level	Password
Operator	А	1111
Controller	А, В	2222
Administrator	A, B, C	1234

The virtual keyboard allows entering desired values by pressing the respective characters and digits. Pressing ENTER confirms and saves the entered value. Pressing CLEAR deletes all entered symbols at the same time, but BS (backspace) – deletes symbols one by one. Pressing Esc (escape) allows exiting the keyboard without saving any changes.

t°C:0.	0 pH:0.00	DO: -0.1 Cas	c. 0 Process Time:	0: 0 :0 🔻 English 🖌 🧲
	Login aw user lete user Change Issword	Date De 22270 Username: Password:	Admin • • •	
qa	w e	r t d f g	yuj hjk	o p €
۞ 6123	z ×	c v	<b>b n m</b> English	· · &

Figure 5.5. The virtual keyboard

In the ADMINISTRATION window, Administrator access level allows to:

• Create new users.

After pressing the NEW USER button, a pop-up window will appear in which it is possible to select the new user's name, password and access level (Privilege – A, B, C). Only C privilege users can create New User, Delete users and Change passwords. B privilege users can operate with every bioprocess controller operation element except the CALIBRATION window. A privilege users can access only the REACTOR, SETTINGS (1<sup>st</sup> & 2<sup>nd</sup> Window), FEEDING, RECIPE and TREND window.

To confirm this action - press ADD USER, see Figure 5.6.

II.	t°C:0.0 pH:0.0	00 DO: -0.1 Casc. 0 (L) Process Time: 0: 0 :0 - English
ස	Login	Alarms Events
	New user	Add New User X
	Delete user	Name:
Ħ	Change password	Password:
<u>k</u>		Select privilege
		Admin Controller Operator
		<u>ок</u> 107
\$	Disable alarms	User: Admin
		11:04:44 A011- Power supply alarm

Figure 5.6. New user window

• Delete User

After pressing the DELETE USER button, a pop-up window will appear in which it is possible to select the desired username, which needs to be deleted. By pressing the DELETE button confirm the action, see Figure 5.7.



Figure 5.7. Delete user window

• Change password.

After pressing the CHANGE PASSWORD button, a pop-up window will appear in which it is possible to select the desired Username, whose password ought to be changed. Enter the new password and press OK to confirm the action, see Figure 5.8.

ų	t°C:0.0 pH:0.00	DO: -0.1 Casc. 0 (L) Process Time: 0: 0: 0: 0 - English
ත	Login	Alarms Events Date Time ACK time Message
	New user Delete user	Change Password X
÷	Change password	Username: Admin •
<u>k~</u>		Password:
		105
Ф	Disable alarms	User: Admin
ply ala	rm	11:04:44 A011- Power sup ?

Figure 5.8. Change password window

To log out of the system the user can press on the LOG OUT button, which is seen in the top right corner of the software interface.

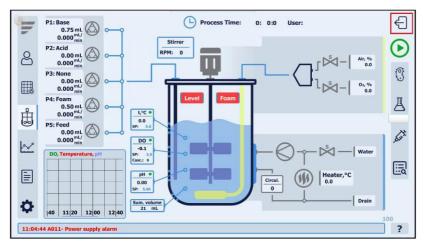


Figure 5.9. Accessing LOG OUT from menu bar

#### 5.3 REACTOR WINDOW

By using the access path MENU  $\rightarrow$  REACTOR open the REACTOR window (see Figure 5.10). Alternatively, the REACTOR window can be accessed by pressing the button with a schematic picture of reactor, highlighted in Figure 5.9. In the REACTOR window all of the most important process parameters can be easily configured and monitored.

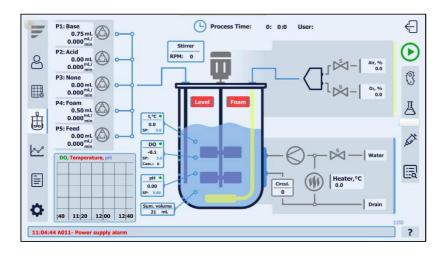


Figure 5.10. REACTOR window

### 6. TEMPERATURE CONTROL

Process temperature control is carried out by supplying a control signal to either the heating element (700 W) or the cooling water electro-magnetic valve. For temperature regulation the respective sensor (Pt100) has to be installed in the bioreactor tank. The heating element and the electro-magnetic cooling water valve are located in the bioprocess controller's thermostat. The circulation pump (also located in the thermostat) maintains the water flow through the bioreactors jacket, which is installed in the bioreactor bottom lid.



Temperature sensors (Pt 100) are pre-calibrated prior to delivery, and repeating of the calibration procedure in unnecessary.

#### 6.1 BIOREACTOR TEMPERATURE CONTROL

To set-up the set-points of the temperature, using the access path: MENU  $\rightarrow$  REACTOR, open the TEMPERATURE SETTING WINDOW, highlighted in Figure 6.1.

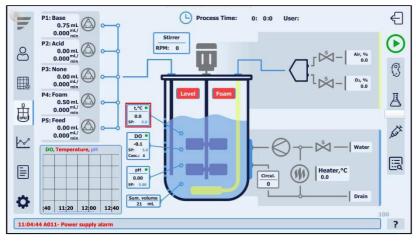


Figure 6.1. Temperature configuration window

Adjust the temperature set-points by clicking on the red digits next to the abbreviation SP and enter the necessary values (highlighted in Figure 6.2), confirm your action by pressing ENTER.

Alternatively, the temperature set-point can be configured in the SETTINGS window. Using the access path MENU  $\rightarrow$  SETTINGS  $\rightarrow$  SETP./LIMITS  $\rightarrow$  PARAMETER SETPOINTS  $\rightarrow$  TEMP. Adjust the setpoints by clicking on the respective digit (highlighted in Figure 6.3).

Limits		Setpoints		Deadzone	
Stirrer min	5 RPM	Temperature	5.0	°C	
Stirrer max	5 RPM	рН	5.00	+/- 5.00	
O2 enrichment max	5.0 %	DO	5.0	%-sat +/- 5.0 %-sat	:
Feed rate min	5.0 %	Filling time	500	Sec	
Feed rate max	0.0 %	Foam pump period	5	Sec	
		Foam pulse length	5	Sec	
		Level pump off delay	5	Sec	
Alarm offset from se	etpoint	Initial volume	5	mL	
		P1 pump productivity	5.000	mL/min	
DO +/-	5.0	P2 pump productivity	5.000	mL/min	
pH +/-	5.00	P3 pump productivity	5.000	mL/min	
Temperature +/-	<u>5.0</u> °C	P4 pump productivity	5.000	mL/min	

Temperature control can be carried out in either Manual or Automatic mode. Note that the water connections and temperature sensor wiring (see Sections 3.4: "SERVICE CONNECTIONS" and 3.5: "VESSEL CONNECTIONS") should be performed prior temperature monitoring and control. Liquid in the reactor should be agitated (see Section 7: "AGITATION CONTROL") to maintain consistent temperature distribution. Using the access path MENU  $\rightarrow$  REACTOR, click on the HEATER or WATER valve symbol (highlighted in 6.3) and select the desired control mode - Manual or Automatic in the pop-up window.

If an element is switched to manual mode a letter M will appear above it in the REACTOR window, highlighted in Figure 6.3. Green colour indicates the currently active operation elements, see Figure 6.3.

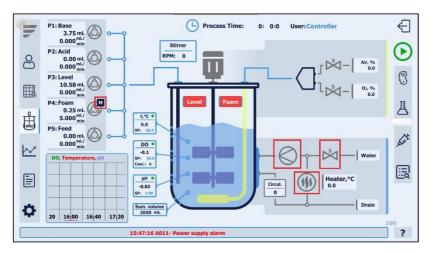


Figure 6.3. Symbols of the circulation pump, water valve and heater

While in Manual mode, the cooling or heating actions can be implemented by switching ON the respective control element (water valve, heater and circulation pump).

While in Automatic mode, automatic temperature control at pre-set set-points is implemented whilst the fermentation process is enabled (see Section 21.3: "STARTING THE PROCESS". The respective control elements operate according to the PID algorithms and individual PID coefficient values (see Section 18.1: "SETTING UP PID PARAMETERS").



Temperature control can be implemented only if liquid flow is present in the thermostat loop. The circulation sensor measures the mentioned flow rate. If the heater is turned on, but no flow is present at-least <u>during</u> 30 seconds, the system will automatically terminate further temperature control. Refer to the TROUBLESHOOTING section for more advise.

### 7. AGITATION CONTROL

The bioreactor agitation specifications:

Stirrer rotational speed interval:	40 - 650 rpm;
Drive type:	magnetic;
Impeller type:	three standard Rushton turbines.

The stirrers rotational speed control can be carried out in either Manual or Automatic mode.

While in Automatic mode the stirrer rotational speed regulation is implemented, if the respective limits (Min/Max) are entered, the values are not equal to each other and the Min parameter is smaller than the Max parameter. The stirrer rotational speed can be regulated within the range determined by the Min and Max parameters (to set them up use the following access path: MENU  $\rightarrow$  SETTINGS  $\rightarrow$  SETP./LIMITS  $\rightarrow$  LIMITS  $\rightarrow$  STIRRER highlighted in Figure 7.2).

While in Manual mode the stirrer can be switched ON or OFF manually in the REACTOR window by entering the respective control element window. It is possible to pre-set a constant agitation rate while in manual mode.

#### 7.1 CONTROL SETTINGS

The stirrer control window can be entered by using the following access path: MENU  $\rightarrow$  REACTOR and pressing the respective symbol. In the stirrer control window it is possible to enter the stirrer's SP value, turn it ON/OFF and monitor its process value (PV), see Figure 7.1. Also, the desired operation mode – Manual/Automatic can be chosen.

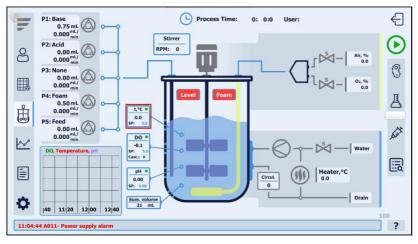


Figure 7.1. Stirrer's control window

The stirrer speed setting adjustment for pO<sub>2</sub> cascade control can be performed using the path: MENU > SETTINGS > PUMPS/CASC. > pO<sub>2</sub> CASCADE. More detailed information about cascade control can be found in Section 7.2: "DISSOLVED OXYGEN (DO) CONTROL BY STIRRER ROTATION RATE" and Section 12: "DISSOLVED OXYGEN (DO) CONTROL". To set-up the Min/Max parameters for stirrer rotational speed control, use the following access path: MENU  $\rightarrow$  SETTINGS  $\rightarrow$  SETP./LIMITS  $\rightarrow$  LIMITS  $\rightarrow$  STIRRER (highlighted in Figure 7.2).

### 7. AGITATION CONTROL

	Limits		Setpoints		Deadzone	
8	Stirrer min	5 R	M Temperature	5.0	°C	
	Stirrer max	5 R	м рн	5.00	+/- 5.00	
	O2 enrichment max	5.0 %	DO	5.0	%-sat +/- 5.0 %-sat	
	Feed rate min	5.0 %	Filling time	500	Sec	
	Feed rate max	0.0 %	Foam pump period	5	Sec	
D			Foam pulse length	5	Sec	
∄			Level pump off delay	5	Sec	
9	Alarm offset from s	etpoint	Initial volume	5	mL	
	DO +/-	5.0	P1 pump productivity	5.000	_mL/min	
~~	pH +/-	5.00	P2 pump productivity	5.000	mL/min	
	Temperature +/-	5.0 %	P3 pump productivity	5.000	mL/min	
=	remperature 17		P4 pump productivity	5.000	mL/min	
Ē						
-			<u> </u>			

Figure 7.2. Stirrer rotational speed Min/Max parameter setting window

#### 7.2 DISSOLVED OXYGEN (DO) CONTROL BY STIRRER ROTATION RATE

In the bioreactor system, DO concentration is controlled via automatic control of the stirrer's rotational speed.

If the SP (Set Point) and DZ (Dead Zone) for the  $pO_2$  value are defined, the stirrer operates in such a way, to maintain the process  $pO_2$  value at: SP  $\pm$  DZ. If the  $pO_2$  value is within the aforementioned range, the stirrer's rotational speed remains constant. If the  $pO_2$  value is out of this range, the agitation rate will be adjusted in respect to the PID algorithm to return the SP to the defined range. For more detailed information, see Section 12: "DISSOLVED OXYGEN (DO) CONTROL".

### 8. AIR/O<sub>2</sub> SUPPLY SETTINGS

The AIR and  $O_2$  gas flow and pressure control equipment is located on the front panel of the bioprocess controller and consists of:

- Gas flow indicators/regulators (rotameters);
- Manometers;
- Pressure regulators (see Figure 8.1).

Rotameters ensure the manual regulation of the respective gas flow rate. Information about rotameter scale calibration (relationship to flow rate in liters per minute) can be found in the technical documentation that is supplied alongside with the equipment.

Pressure regulators ensure the regulation of the respective gas pressure before entering the rotameter (manometers serve as pressure indicators). Pressure regulators also allow manual regulation of the respective gas flow. Normally, gas flow rate regulation is carried out by rotameters, but in some cases using pressure regulators, it is possible to adjust the pressure of the inlet gas (to 0.05 MPa or higher), in result increasing or decreasing the gases flow rate.

Manometers enable visual monitoring of the respective gases pressure (in MPa) before entering the rotameter.

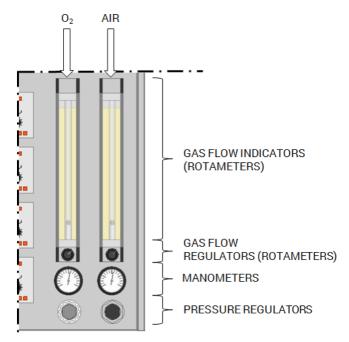


Figure 8.1. Gas flow control equipment

To set-up the  $air/O_2$  supply, follow the instructions listed further:

- Access the REACTOR window and locate the AIR and O<sub>2</sub> sections in the top-right corner of the window. By pressing the respective gas valve symbol, the control window for the respective gas will appear, see Figure 8.2;
- 2) After switching on the Manual control of the respective valve, enable the respective gas flow by turning ON the valve;

- 3) Based on the respective manometer reading, set-up the desired gas pressure using the pressure regulator (see Figure 8.1);
- 4) Set-up the desired gas flow rate using the respective rotameter (taking into account the calibration and correction values based on pressure, temperature and density of the applied gas).

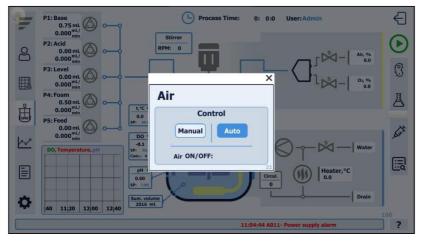


Figure 8.2. Gas control window

### 9. Two gas supply control

The bioreactor system provides possibility of mixing two gases  $(air/O_2)$  to obtain a desired  $O_2$  concentration in the inlet gas flow. This can be implemented in two ways: (1) manual two gas mixture supply and (2) two gas mixture supply via automated control of DO (pO<sub>2</sub>), see Section 12: "DISSOLVED OXYGEN (DO) CONTROL".

The principle of setting-up mixing of two gasses is similar to that described in Section 8: "AIR/O<sub>2</sub> SUPPLY SETTINGS" (in the case of (1) manual two gas mixture supply), and in Sections 12: "DISSOLVED OXYGEN (DO) CONTROL and 15: "DISSOLVED OXYGEN (DO) CASCADE CONTROL", (in the case of (2) two gas mixture supply via automated control of DO (pO2)). In such cases only the types and combinations of the respective gasses will differ. To exercise such an option, please see the respective sections (Sections 8: "AIR/O<sub>2</sub> SUPPLY SETTINGS", 12: "DISSOLVED OXYGEN (DO) CONTROL" and 15: "DISSOLVED OXYGEN (DO) CONTROL".

9.1 DISSOLVED OXYGEN CONTROL BY MIXING OF AIR/O<sub>2</sub>

The automated Air/O<sub>2</sub> mixtures control is performed by adjusting the respective gas valves open time. The control is implemented in such manner, so that O<sub>2</sub> concentrations range of 0 – 100 % can be achieved while the summary flow remains constant.

When the  $O_2$  concentration in the inlet flow needs to be increased, the open time of the  $O_2$  gas valve is increased, while the Air gas valves open time is decreased proportionally. This results in  $O_2$ concentration growth while the summary gas flow remains constant. If the  $pO_2_PV$  value remains > than the  $pO_2_SP$  value and the  $O_2$  gas valves open time reaches its Max limit, then the  $pO_2_PV$  value remains < than the  $pO_2_SP$  value and the  $O_2$  gas valves open time reaches its Min limit, then the  $pO_2_PV$  value remains < than the  $pO_2_SP$  value and the  $O_2$  gas valves open time reaches its Min limit, then the  $pO_2_PV$  value remains < than the  $pO_2_SP$  value and the  $O_2$  gas valves open time reaches its Min limit, then the  $pO_2_PV$  value control will be implemented by previous cascade (if the next cascade was chosen).

To set-up the Max parameter for oxygen enrichment control, use the following access path: MAIN MENU  $\rightarrow$  SETTINGS (1<sup>st</sup> WINDOW)  $\rightarrow$  LIMITS  $\rightarrow$  O<sub>2</sub> enrichment max (highlighted in Figure 9.1).

Limits			Setpoints	Setpoints Dea		
Stirrer min	100	RPM	Temperature	36.0	°C	
Stirrer max	800	RPM	pH	7.00	+/- 0.20	
O2 enrichment max	30.0	%	DO	50.0	%-sat +/- 5.0	%-sat
Feed rate min	50.0	%	Filling time	30	Sec	
Feed rate max	0.0	%	Foam pump period	10	Sec	
			Foam pulse length	3	Sec	
<u></u>			Level pump off delay	10	Sec	
Alarm offcet from	cetnoint		Initial volume	2000	mL	
Alarm offset from setpoint		P1 pump productivity	5.000	mL/min		
DO +/-		_	P2 pump productivity	5.000	mL/min	
pH +/-		_	P3 pump productivity	5.000	mL/min	
Temperature +/-	0.1	°C	P4 pump productivity	5.000	mL/min	
						User: Admir

Figure 9.1. Settings for O<sub>2</sub> enrichment

### **10.PUMP CONTROL**

By default, the bioreactor system includes a four peristaltic pump unit (see Figure 10.1) for pH, foam, medium level regulation and substrate addition (feeding).

#### 10.1 TUBING

In order to mount the peristaltic pump tubes into the pump head, carry out the steps described below:

- 1) Cut the silicone tubes in a desired length. Their exterior diameter and wall thickness should not exceed 6-8 mm and 1.5 mm, respectively;
- 2) Open the peristaltic pump's head by lifting up the lid. Place the silicone tube around the rotating part of the pumps head and place both ends into their outlets;



Bioreactor's peristaltic pumps operate clockwise in default.

- 3) Close the pump head with an installed silicone tube by lightly pressing the lid down until you hear a click;
- 4) Connect one end of the silicone tube to the titrant bottle and connect the other end to the desired bioreactor port.

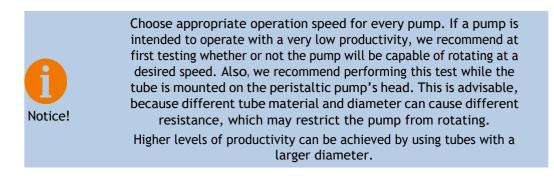
#### 10.2 PUMP PRODUCTIVITY

The productivity of each peristaltic pump is determined during the calibration process (see Section 10.4: "PUMP CALIBRATION"). See Figure 10.1.

ıt

Figure 10.1. Peristaltic pump productivity settings

The pump productivity settings correspond to each individual pumps liquid transfer rate, which will be maintained in case if the pump will be enabled by the system during pH, Level and Foam regulation.



#### 10.3 PUMP CONFIGURATION

To set-up the productivity of each peristaltic pump (excluding the feeding pump), use the following access path: MAIN MENU  $\rightarrow$  SETTINGS (1<sup>st</sup> WINDOW)  $\rightarrow$  SETPOINTS  $\rightarrow$  P1-P4 pump productivity, see Figure 10.2.

I	t°C:0.0	pH:0.00	DO:-0.1	Casc. 0	Process	s Time: 0: 0 :0		Ð
8		Da	bration date: y. Month. Year 7 6 2022	Pump conf 1. Base	iguration Define P1	DO cascade 1. Stirrer On		
			6 6 2022	2. Acid	Define P2	2. 02 enr-t On	Off	
₿	1		6 6 2022 6 6 2022	3. Level 4. Foam	Define P3 Define P4	3. Feed On	Off	1
6	$\left  \right $		6 6 2022 1 1 1970	5. Feed	Define P5			1
			1 6 2022					
•				0 •	0		User: Admin	113
					11:04:	44 A011- Power sup	ply alarm	?

Figure 10.2. PUMPS and pO<sub>2</sub> CASCADE control window

In the pump configuration menu it is possible to define, what function each individual pump will carry. To configure a pump press the respective button (P1, P2, P3, P4 or P5), then select the desired function Base, Acid, Feed, etc. Keep in mind that you can choose only one pump for a specific function.

#### 10.4 PUMP CALIBRATION

Follow the instructions listed below before performing pump calibration:

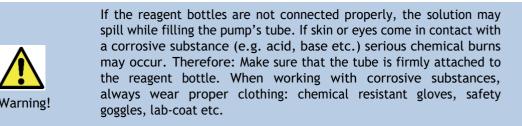
1) Mount the tube, which is intended to be used on the desired peristaltic pump head and attach the reagent bottle to the suction end of the tube;



When inserting the tubes into the pump head, please remember that the peristaltic pumps are operating clockwise.

- Fill the tube with a solution that is intended to be used for pump calibration. Volume, which is pumped during the calibration procedure, should be measured by a precise measuring cylinder or scales (when using scales, keep in mind to calculate the correct volume from mass);
- Access the bioprocess controllers REACTOR window. Set the pump, which is intended for calibration (base, acid, antifoam, level or feed (P1-P5)) to automatic mode (click on the respective pump symbol and press AUTO);

4) Open the calibration window by using the access path MENU  $\rightarrow$  SETTINGS (2<sup>nd</sup> WINDOW)  $\rightarrow$  CALIBRATION;



5) Use buttons P1, P2, P3, P4, and P5 to select the desired pump for calibration (see Figure 10.3). The P5 pump is the external pump\* (controlled by an analogue signal), pumps P1 – P4 are built into the bioprocess controller;

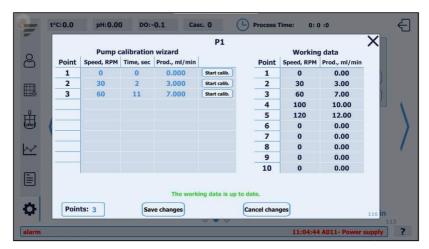


Figure 10.3. Pump calibration window

- 6) In the calibration window define the desired amount of calibration points and the respective speeds and calibration time for each point (see Figure 10.3);
- 7) Pump calibration point amount selection depends on the pre-set function of the pump in case if the pump is used for maintaining pH, Foam and Level, it is recommended to choose at-least three calibration points. For feeding at-least seven calibration points are recommended;
- 8) By pressing the START CALIBR. button the calibration procedure enables. During a pre-defined amount of time the pump operates using the defined settings (see Figure 10.4);
- 9) Remaining Time: shows the remaining time of the calibration cycle;
- 10) After calibration is complete, enter the pumped volume in *ml* into the respective section of the calibration window (Volume).
- By pressing the Save measurement button the user can save the calibration data (see Figure 10.5). By pressing the Cancel calibration button the user can discard the newly entered calibration values.

	Pump	alibration	wizard	P1	Working data
Point			Prod., ml/min		Point Speed, RPM Prod., ml/min
1	0	0	0.000	Start calib.	
2	30	60	3.000	Calibration	Calibration in
3	60	50	7.000	Start calib.	Cancel       Remaining time:     94 %       Volume:     0.000 ml       Save     Cancel       measurement     Calibration       10     0     0.00
Poin	ts: 3	Sa	The worki	ing data is up I	to date.

Figure 10.4. Pump calibration procedure

- 12) After the calibration of all envisioned points has been carried out, the user has to save the calibration data to the system by pressing the Save Changes button. Alternatively, all changes and calibration data can be discarded by pressing the Cancel Changes button (see Figure 10.6).
- 13) To finish the calibration procedure close the calibration wizard's window.

9	t°C:0.0	pH:0.00	) DO:-	0.1 Cas	c. 0	Process Time: 0: 0 :0	Ð
8	Point		alibration Time, sec	wizard Prod., ml/min	P1	Working data Point Speed, RPM Prod., ml/min	<
	1	0	0	0.000	Start calib.		
	2	30	60	3.000	Calibration	Point calibration finished.	
	3	60	60	7.000	Start calib.		
						Enter the volume. Remaining time: 0 % Volume: 0,000 ml masurement Cancel calibration 10 0 0.00	$\left \right\rangle$
				The worki	ng data is u	p to date.	
0	Poin	ts: 3	Sav	e changes		Cancel changes	36 <b>in</b>
					19. <b>1</b> 19		113
						14:44 A011- Power supply alarm	

Figure 10.5. Pump calibration procedure finished

	Pump	calibration	wizard	P1		Working	n data	×
Po	int Speed, RPM	1	1		Point	1	Prod., ml/min	
	L 0	0	0.000	Start calib.	1	0	0.00	
	2 30	60	20.000	Start calib.	2	30	3.00	
	60	60	7.000	Start calib.	3	60	7.00	
					4	100	10.00	
					5	120	12.00	
					6	0	0.00	
					7	0	0.00	
					8	0	0.00	
					9	0	0.00	
					10	0	0.00	
	Points: 3	Say	Calibration tab Do you war	le data have be nt to save the c		ges		116 in

Figure 10.6. Saving pump calibration data

#### 10.5 PUMP CONTROL FROM THE BIOPROCESS CONTROLLER

Pump control from the bioprocess controller can be implemented in two ways: manual (Manual) or automatic (Auto). Open the REACTOR window and navigate to the required pump control window by clicking on the respective symbol (see Figure 10.7). By selecting Manual the option of enabling the pump in manual mode is provided. If the Auto mode is selected, the pump manual controls are suppressed and it will operate only during the fermentation process, in accordance with the respective control settings.

Additionally, the user can reset the pumped volume value within the pump control window by pressing the reset button.

The pump can be automatically enabled to operate with the maximal rotation rate by pressing the fast forward button, within the pump control window.

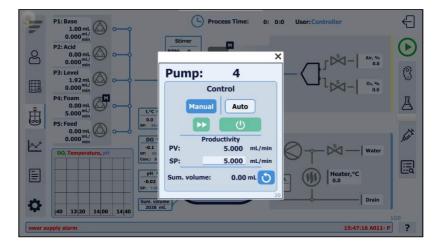
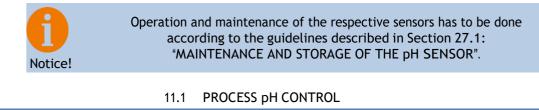


Figure 10.7. Pump control window

## 11. pH CONTROL

The pH value is maintained automatically at a pre-set level by means of base or acid addition to the bioreactors medium using the bioprocess controller's peristaltic pumps (see Section :10 " PUMP CONTROL").



To access the pH control window, open the REACTOR window, locate the pH section (highlighted in Figure 11.1) where the SP value can be set.

Or use the following access path: MENU  $\rightarrow$  SETTINGS  $\rightarrow$  SETP./LIMITS  $\rightarrow$  PARAMETER SETPOINTS  $\rightarrow$  pH to adjust the parameter set-point.

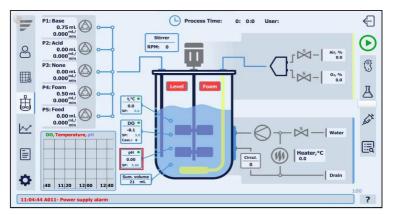


Figure 11.1. Window for setting the process pH value

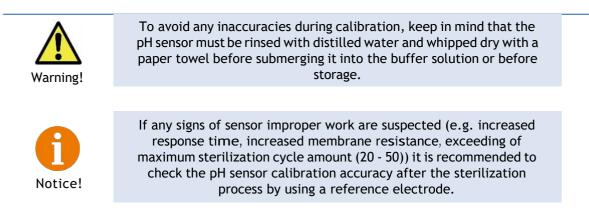
Detailed information on process control settings, including pH control, can be found in Section 21.1: "CONTROLLER SETTINGS FOR STARTING THE PROCESS".

Limits			Setpoints		De	adzone	2
Stirrer min	100	RPM	Temperature	36.0	°C		
Stirrer max	800	RPM	pH	7.00	+/-	0.20	
O2 enrichment m	ax 30.0	%	DO	50.0	%-sat +/-	5.0	%-sat
Feed rate min	50.0	%	Filling time	30	Sec		
Feed rate max	0.0	%	Foam pump period	10	Sec		
			Foam pulse length	3	Sec		
			Level pump off delay	10	Sec		
Alarm offset f	rom setnoint		Initial volume	2000	mL		
			P1 pump productivity	5.000	mL/min		
DO	+/	_	P2 pump productivity	5.000	mL/min		
pH	+/- 0.20	_	P3 pump productivity	5.000	mL/min		
Temperature	+/	°C	P4 pump productivity	5.000	mL/min		
							User: Admin

Figure 11.2. Window for setting the process pH value

11.2 CALIBRATION OF THE PH SENSOR

For measurement reliability during the fermentation process, it is strongly recommended to calibrate the pH sensor before each process. Before performing the calibration procedure, two buffer solutions should be prepared.



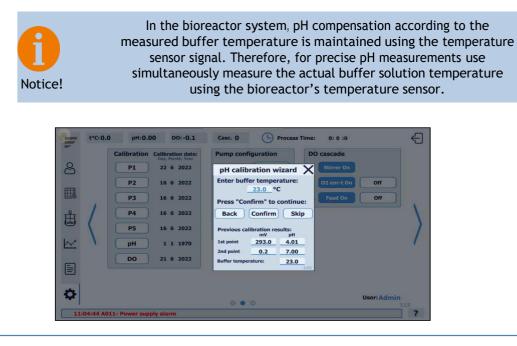
In order to calibrate the pH sensor, follow the instructions outlined further:

1) By using the access path MENU  $\rightarrow$  CALIBR.  $\rightarrow$  pH, open the pH calibration wizard (see Figure 11.3);

-	t°C:0.0 pH:0.00 DO:-0.1	Casc. 0 (L) Process Time: 0: 0 :0	Ð
පී	Calibration Calibration date: Day, Month. Year P1 22 6 2022 P2 16 6 2022	Pump configuration DO cascade pH calibration wizard X Choose the type of calibration: 02 enr-t On 0ff	
	P3 16 6 2022	Correction Calibration Feed On Off	
₿	P4 16 6 2022 P5 16 6 2022	Previous calibration results: mV pH 1st point 293.0 4.01 2nd point 0,2 7.00	
	pH         1         1         1970           DO         21         6         2022	Buffer temperature: 23.0	e
\$		🛛 🔹 🔿 User: Adm	in 113
		11:04:44 A011- Power supply alarm	?

Figure 11.3. pH Calibration wizard

- 2) Two options for pH calibration have been envisioned: (1) pH Correction and (2) pH Calibration;
- 3) By selection pH Calibration proceed to the pH calibration menu;
- 4) Enter the buffer solution temperature in the pH calibration window by clicking on the digits (which are indicated under the title "Enter buffer temperature") (see Figure 11.4);



- 5) The user has three option to navigate through the pH calibration wizard: Back, Confirm and Skip. By pressing the Back button the user can return to the previous calibration window (all entered data will be saved). By pressing the Confirm button the user can proceed to the next calibration window. By pressing the Skip button the user can skip the current calibration window (without saving any new data) and proceed to the next calibration window;
- 6) After the correct buffer temperature has been entered press Confirm;
- 7) In the next window, it is required to enter the first buffer solution pH value (see Figure 11.5);
- 8) Immerse the sensor into the buffer solution, enter its pH value and wait until the mV readings stabilize;
- 9) When the mV value has stabilized press Confirm;
- pH calibration wizard for entering the second buffer solution's pH value will appear (see Figure 11.6);

	Calibration Calibration date: Day, Month. Year	Pump configuration D	O cascade
	P1 22 6 2022	pH calibration wizard 🗙	Stirrer On
	P2 16 6 2022	Enter 1st buffer: 4.01 pH	02 enr-t On Off
	P3 16 6 2022	Wait for stable mV signal:	Feed On Off
1	P4 16 6 2022	412.5 mV	
	P5 16 6 2022	Back Confirm Skip	
	pH 1 1 1970	Previous calibration results:	
	DO 21 6 2022	1st point 4.01	
		2nd point     0.2     7.00       Buffer temperature:     23.0	
		161	

Figure 11.5. pH calibration wizard for calibration of the first buffer solution

- 11) For the second point calibration it is recommended to use buffer solution with a pH value that is close to the isopotential point (~7 pH);
- 12) Immerse the sensor into the second buffer solution, enter its pH value and wait until the mV readings stabilize. When mV value has stabilized click Confirm;
- 13) After pressing READY a notification will appear: "Calibration Ok!";
- 14) To save the new calibration data press the Save button.
- 15) By selection pH Correction function the user can access the correction wizard, where it is possible to re-calibrate the sensor during a running cultivation with the help of a reference electrode.
- 16) Take a sample of the cultivation medium. Place a reference pH electrode into the sample and measure the pH of the solution;
- 17) Enter the pH value measured by the reference electrode into the pH correction wizard.
- 18) By pressing the Confirm button the pH correction procedure is finalized

IL	t°C:0.0	D pH:0.0	0 DO:-0.1	Casc. 0 (L) Process Time: 0: 0 :0	Ð
A SPACE		Calibration	Calibration date: Day, Month, Year	Pump configuration DO cascade	
8		P1	22 6 2022	pH calibration wizard X Stirrer On	
		P2	16 6 2022	Enter 2nd buffer: 02 enr-t 0n Off	
		P3	16 6 2022	7.00 pH       Wait for stable mV signal:	
₿		P4	16 6 2022	mV	
		P5	16 6 2022	Back Confirm Skip	
100°	1	рН	1 1 1970	Previous calibration results:	
		DO	21 6 2022	1st point 4.01	
				2nd point 0.2 7.00	
				Buffer temperature: 23.0 162	
•				User: Admin	
5				11:04:44 A011- Power supply alarm	?
- Comment					

Figure 11.6 pH calibration wizard for calibration of the second buffer solution

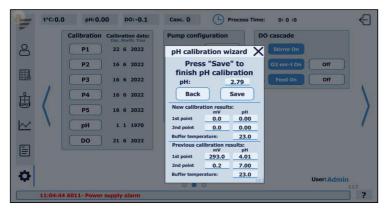


Figure 11.7 pH calibration wizard with completed calibration

1L	t°C:0.0 pH:-0.01 DO:-0.1	Casc. 0 Process Time: 0: 0: 0: 0	€
	Calibration Calibration date: Dep Manni, Vari P1 22 6 2022 P2 16 6 2022 P3 16 6 2022 P4 16 6 2022 P5 16 6 2022	Pump configuration     DO cascade       pH correction wizard     Stirrer On       pH:     -0.01       Corrected pH:     0.00       Delta pH:     -2.58       Back     Confirm       vr. recev     Stirrer V	$\rangle$
	pH         22         6         2022           DO         21         6         2022	User: Admin	1
	11:04:44 A011- P	ower supply alarm	?

Figure 11.8. pH correction wizard

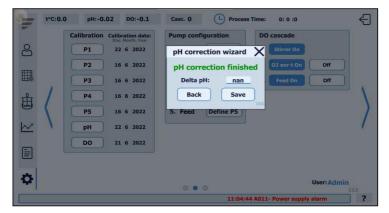


Figure 11.9. pH correction finished

## 12. DISSOLVED OXYGEN (DO) CONTROL

The dissolved oxygen (DO) level in the culture medium is measured as dissolved oxygen partial pressure  $(pO_2)$ .  $pO_2$  is expressed in % from maximally possible oxygen concentration that is determined during sensor's second point (maximal oxygen saturation (100 %)) calibration. In the bioreactor system, DO can be controlled via automatically manipulated variable of: (1) stirrer

rotation speed, (2) inlet air enrichment rate of  $O_2$  flow (see Section 15: "DISSOLVED OXYGEN (DO) CASCADE CONTROL"), (3) and substrate feeding rate.



Handling of the pO<sub>2</sub> sensor has to be done according to the instructions described in Section 27.2: "MAINTENANCE AND STORAGE OF THE pO<sub>2</sub> SENSOR".

To access the  $pO_2$  control window, open the REACTOR window, locate the  $pO_2$  section (highlighted in Figure 12.1) where the SP value can be set.

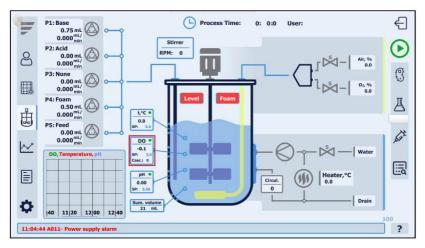


Figure 12.1. Window for setting the processes  $pO_2$  value

Or use the following access path: MENU  $\rightarrow$  SETTINGS (1<sup>st</sup> WINDOW)  $\rightarrow$  SETPOINTS to adjust the parameter set-point (see Figure 12.2).

T	t°C:0.0 pH:0.00 DO:-0.1	Casc. 0	Process	s Time: 0:	0:0		÷
	Limits	Setpoints		De	adzone	E I	
පි	Stirrer min 100 RPM Stirrer max 800 RPM	Temperature pH	36.0 7.00	°C +/-	0.20	·	
	02 enrichment max 30.0 %	DO	50.0	%-sat +/-	5.0	%-sat	
	Feed rate min         50.0         %           Feed rate max         0.0         %	Filling time	30	Sec			
		Foam pump period Foam pulse length	10	Sec			1
₿		Level pump off delay	10	Sec			
6	Alarm offset from setpoint	Initial volume	2000	mL			
		P1 pump productivity	5.000	mL/min			
000	DO +/- 5.0 pH +/- 0.20	P2 pump productivity	5.000	mL/min			
	Temperature +/- 0.1 °C	P3 pump productivity	5.000	mL/min			
-		P4 pump productivity	5.000	mL/min			
		ļ					
<b>V</b>		• 0 0				User: A	
·	11.04.4						109
	11:04:4	4 A011- Power supply a	larm				f

Figure 12.2. Window for setting the processes DO value in SETTINGS

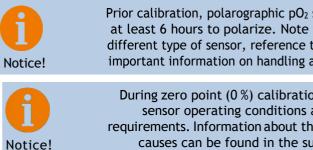
Detailed information on process control setting selection, including pO<sub>2</sub> control setting selection, is listed in Section 20.:"CONTROLLER SETTINGS FOR STARTING THE PROCESS".

### 12.1 GENERAL INFORMATION ABOUT THE PO2 SENSOR'S CALIBRATION

In general,  $pO_2$  sensor's calibration procedure should be carried out after sterilization. The test calibration prior sterilization is advised for inspection of the sensor and system's operating conditions.

The calibration procedure can be performed in two ways, i.e. using (1) two point or (2) one point

linearization. While performing the upper mentioned actions, the sensor has to be subjected to either oxygen saturated and/or oxygen-free environments. Two point calibration is recommended when the sensor is being calibrated for the first time. Occasional two point calibration is recommended to identify any measurement errors, which can occur while using the sensor.



Prior calibration, polarographic pO<sub>2</sub> sensors require a time period of at least 6 hours to polarize. Note that in case if you are using a different type of sensor, reference to the sensor user manual about important information on handling and maintaining the equipment.

During zero point (0%) calibration it is possible to evaluate the sensor operating conditions and potential maintenance requirements. Information about the possible malfunctions and their causes can be found in the supplied sensor user manual.

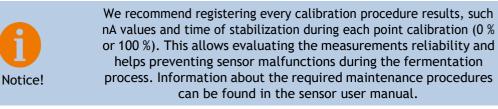
Ensuring oxygen-saturated environment:

Sensor exposure to air. Affix a clean and dry sensor to a stand or in an aerated bioreactor's tank without any liquid. This method can be used before and after sensor sterilization.

Sensor exposure to agitated and aerated bioreactor environment. This method is best suited for simulation of oxygen-saturated environment in conditions, which most closely reproduce the maximal oxygen concentration, which can be achieved within the fermentation process. Distilled water, culture medium or fermentation broth can be used as a liquid phase. Maintain the liquid temperature and vessel's inner pressure at values as close as possible to those, which are to be used during the fermentation process. Agitation and aeration rates should be set-up as maximal limits used in the process, taking into account the culture tolerance to mechanical damage! Typically, stirrer's rotational speed of 300 rpm and 5 - 10 slpm of aeration can be applied if the process will run using shear stress resistant microorganism (e.g. bacteria, yeast etc.). This method can be used before and after sensor sterilization.

Ensuring oxygen-free environment:

Sensor exposure to the bioreactor environment aerated with nitrogen  $(N_2)$  gas. Distilled water, culture medium or fermentation broth can be used as a liquid phase. Typically, stirrer rotation speed of 500 rpm and 2 - 3 slpm of nitrogen gas can be applied. Under these conditions, oxygen displacement normally happens within 5 - 10 min. This method can be used before and after sensor sterilization.



### 12.2 TWO POINT CALIBRATION

### 0 % point calibration

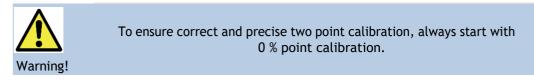
Choose one of the methods described in Section 12.1: "GENERAL INFORMATION ABOUT THE pO2 SENSOR'S CALIBRATION" - "Ensuring oxygen-free environment" and follow the instructions listed below to carry out the  $pO_2$  sensor calibration.

1) Use the access path MENU  $\rightarrow$  SETTINGS (2<sup>nd</sup> WINDOW)  $\rightarrow$  CALIBRATION  $\rightarrow$  DO, to open the DO calibration wizard (see Figure 12.3) and select the desired calibration method;

t°C:0	.0 pH:-0.02 DO:-0.1	Casc. 0 (b) Process Time: 0: 0 :0	€
- 00 III - 10 2	Calibration         Calibration         Calibration         date: Day, Meeth.           P1         22         6         2022           P2         16         6         2022           P3         16         6         2022           P4         16         6         2022           P5         16         6         2022	Pump configuration     DO cascade       DO calibration wizard     X       1 point or 2 point calibration:     Stirrer On       1 Point     2 Point       Press "Confirm" to continue:     Confirm       Previous calibration results:     %       1st point     65.8	>
¢	pH 22 6 2022 DO 21 6 2022	2nd point	?

Figure 12.3. pO<sub>2</sub> calibration wizard

 Choose 2 Point, then - press Confirm. Notification with instructions for placing the electrode in an oxygen-free environment will appear, enter the value of the first calibration point (0 %) (see Figure 12.3);



- 3) The user has three option to navigate through the DO calibration wizard: Back, Confirm and Skip. By pressing the Back button the user can return to the previous calibration window (all entered data will be saved). By pressing the Confirm button the user can proceed to the next calibration window. By pressing the Skip button the user can skip the current calibration window (without saving any new data) and proceed to the next calibration window.
- 4) Subject the electrode to an oxygen-free environment and wait for the nA reading to stabilize (usual in the range of 0 1.5 nA), see Figure 12.4;
- 5) Press Confirm, this will bring up the next calibration wizard with instructions saying to immerse the electrode in an oxygen-saturated environment (100 % point calibration), see Figure 12.5.

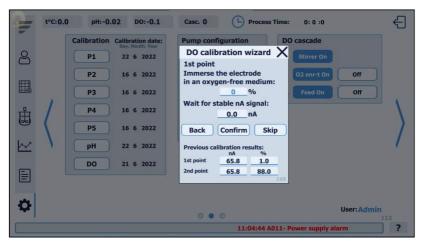


Figure 12.4. pO<sub>2</sub> two point calibration wizard (first step)

4	t°C:0.0	pH:-0.	02 DO:-0.1	Casc. 0 Process Time: 0: 0 :0	3
		Calibration	Calibration date:	Pump configuration DO cascade	
0		P1	22 6 2022	DO calibration wizard X	
		P2	16 6 2022	2nd point Immerse the electrode in an oxygen saturated medium: 02 enr-t 0n Off	
		P3	16 6 2022	100 % Feed On Off	
₿	1	P4	16 6 2022	Wait for stable nA signal:	
		P5	16 6 2022	Back Confirm Skip	6
<u>k</u> ~	N	рН	22 6 2022	Previous calibration results: nA %	
Ē		DO	21 6 2022	1st point         65.8         1.0           2nd point         65.8         88.0	
\$				O • O User: Admin	
		1	1:04:44 A011- Po	wer supply alarm	

Figure 12.5. pO<sub>2</sub> two point calibration wizard (second step)

### 100 % point calibration

Choose one of the methods described in Section 12.1: "GENERAL INFORMATION ABOUT THE  $pO_2$  SENSOR'S CALIBRATION" – "Ensuring oxygen-saturated environment" and follow the instructions listed below to carry out the  $pO_2$  sensor calibration.

- Subject the electrode to an oxygen-saturated environment and wait for the nA reading to stabilize (usual in the range of 40 - 80 nA);
- 2) Press READY (see Figure 12.4) and a notification window "Calibration OK!" will appear;
- 3) Press EXIT in order to save the calibration data and exit the  $pO_2$  Calibration wizard.

### 12.3 ONE POINT CALIBRATION

#### 100 % point calibration

Choose one of the methods described in Section 12.1: "GENERAL INFORMATION ABOUT THE  $pO_2$  SENSOR'S CALIBRATION" – "Ensuring oxygen-saturated environment" and follow the instructions listed below to carry out the  $pO_2$  sensor calibration:

- 1) Use the access path MENU  $\rightarrow$  CALIBR.  $\rightarrow$  pO<sub>2</sub> to open pO<sub>2</sub> calibration wizard (see 12.3);
- 2) Choose 1 Point, then press Confirm;
- 3) Perform steps 2-4 that are described in Section 12.2: "TWO POINT CALIBRATION" 100 % point calibration.

## 13. FOAM CONTROL

Foam regulation can be carried out by supplying an anti-foam agent to the bioreactor's environment using one of the bioreactor's peristaltic pumps. Control is implemented using the respective conductivity sensor, which supplies a signal to the bioprocess controller when the foam rises to a pre-set level. If the sensor signal becomes active; within the REACTOR window the Foam alarm is signalized. After the bioprocess controller receives the sensor signal, the respective pump starts operating and pumps antifoam to the bioreactor environment according to the pre-set settings until the signal becomes inactive.

### 13.1 FOAM CONTROL PRINCIPLE

The foam sensor should be installed according to the peculiarities of each specific process. The installation includes configuration of the distance (the optimum distance is around 5 – 10 cm) between the fermentation environment and the lower part of the foam sensor. The antifoam pump operation conditions can be adjusted using the access path MENU  $\rightarrow$  SETTINGS (1<sup>st</sup> WINDOW)  $\rightarrow$  SETPOINTS (see Figure 13.1).



Figure 13.1. Foam pump period settings

The user can define both the Foam pump period and Foam pulse length. The respective pump, upon receiving a signal from the bioprocess controller will operate in pulses, where each pulse time is equal to the Foam pulse length and the pause between pulses is equal to the difference between the Foam pulse length and the Foam pump period, e.g. in the given example the pump will operate for 3 seconds after each 7 seconds.

## 14. LEVEL CONTROL

Level regulation is carried out in a similar way as in the case of foam level control, i.e. by the conductivity sensor signal. If the sensor signal becomes active; within the REACTOR window the Level alarm is signalized. Reaction medium will be pumped out of the bioreactor through a chemostat tube. A respective port has to be mounted on the upper bioreactor lid for level control implementation. The end of the chemostat tube has to be submerged in the reaction medium.

#### 14.1 LEVEL CONTROL PRINCIPLE

The foam sensor should be installed according to the peculiarities of each specific process. The bioreactor allows a time delay to be set for the level control algorithm. The level pump delay is applied in the time period between the activation of the level signal and the activation of the LEVEL pump. To set-up the level pump off delay, use the access path: MENU  $\rightarrow$  SETTINGS (1<sup>st</sup> WINDOW)  $\rightarrow$  SETPOINTS (see Figure 14.1).

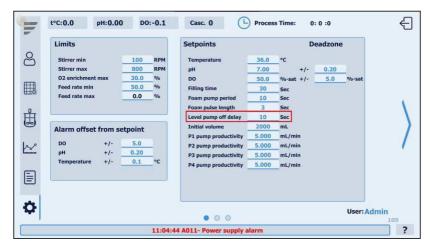


Figure 14.1. Level pump off delay settings

In the Bioreactor system, DO can be controlled via automatically manipulated variables (cascades) of (1) stirrer rotation speed, (2) inlet air enrichment rate of  $O_2$  flow, (3) and substrate feeding rate.

### 15.1 THE PRINCIPLES OF ESTABLISHING THE PO<sub>2</sub> CASCADE CONTROL

The general pO<sub>2</sub> cascade control principles are described further. At first, the SP (Set Point) and DZ (Dead Zone) are set for the necessary pO<sub>2</sub> control range. The respective performance mechanism works on the process in such a way that the pO<sub>2</sub> value is maintained within the range of SP - DZ <  $pO_2 < SP + DZ$ . If the pO<sub>2</sub> value is within the aforementioned range, no control action of manipulated variable takes place. If pO<sub>2</sub> value is beyond such range, the manipulated variable is being controlled according to the PID algorithm. In all cases, except for the oxygen enrichment impulse control, the manipulated variable is controlled by a proportional control signal (between 4 - 20 mA or 0 - 10 V). The regulation is suspended in each cascade when the minimum or maximum limiting value has been reached. The control of all of the aforementioned variables can be combined into pO<sub>2</sub> cascade control.

 $pO_2$  control may take place with different cascades. The control of each cascade takes place according to the described types. Any of the described cascades can be selected and any order for their sequencing can be established.

Cascade control is working in line with the following principles:

- Appropriate cascade sequence of manipulated variables should be defined before process. The particular manipulated variable control happens until upper limit of its set-point or lower limit for cascades no. 2 - 3 is reached. When the limiting set-point is reached, the transition to the next or previous cascade takes place depending on which (maximum or minimum) limiting value has been reached. Transition to the next cascade cannot take place if the current cascade is the last one;
- 2) Regulation begins in a specific cascade when a certain  $pO_2$  and manipulated variable limits is reached. When a limiting value has been reached, the transition to the next or previous cascade will take place. The manipulated variable continues in operation in the following cascade with its preceding status. The only exception is when the following cascade is "substrate feeding". In such an event the cascade begins with the productivity of the feeding pump, which was actual from the particular feeding profile. If feeding was not active according to the feeding profile, then feeding shall begin in this cascade with some of the limiting values (minimum or maximum in percents from feeding pump's maximal productivity).

15.2 PO<sub>2</sub> CASCADE CONTROL

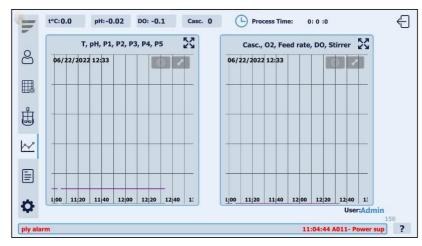
Access  $pO_2$  cascade control by using the path: MENU  $\rightarrow$  SETTINGS(2^{nd} window)  $\rightarrow$   $pO_2$  CASCADE.



Figure 15.1. PUMPS and pO2 CASCADE control window

The given window offers in  $pO_2$  cascade control used manipulated variable of Stirrer speed,  $O_2$  enrichment and Feed rate, configuration (see Figure 15.1). To choose manipulated variable order use buttons C1, C2, C3, and select appropriate cascade performance element.

# 16. PROCESS TRENDS



To open the trends menu use the access path MENU  $\rightarrow$  TRENDS, see Figure 16.1.

Figure 16.1. TRENDS window

The TRENDS window displays the changes in the dynamics of process parameters (temperature, pH,  $pO_2$ , stirrer, pumps, etc.), by clicking on the maximise buttons for the 1<sup>st</sup> and 2<sup>nd</sup> trend fields the user can gain access to a larger window, which displays the respective trends.

Within each trend window the user can:

- Configure the scale of the Y axis for each individual parameter (see Figure 16.2);
- Change the visibility of each parameter (see Figure 16.4) accessed by pressing the cog button on the Trend field (see Figure 16.3).

Change the visibility of the Y axis for each individual parameter (see Figure 16.5) accessed by pressing the cog button on the Trend field (see Figure 16.3).



Figure 16.2. Y axis scale configuration window



The user can navigate through the trend field by dragging the image left and right. Additionally it is possible to magnify a particular region by spreading the image using two fingers.

t°C:0.0	pH:- Cancel	Option	Done :0
06/22/2022	12:34 FILE SELECTION		Days ago
	1st latest file (20220622)		
	2nd latest file (20220621	)	Temp.,°C
			pH 0.00
			Level volume 0.00
			Fead volume 0.00
	TREND DISPLAY SETTING		
	Channel Visibility		Y scale
	Y Scale		Off BACK
,	Disable Y-axis scrolling	(	
1;00 11;10	11:20	leset to default	: User:Admin

Figure 16.3. Trend configuration menu

L.	t°C:0.0 pH:-	Option	Channel Visibility		:0	Ĵ
	06/22/2022 12:35				Days ago	
8		Temperature			$\Theta \bullet \bullet$	
		рН			Temp.,°C	
		P5 volume			рн <u>0.00</u> Вахе уоште 0.00	
		P1 volume			0.00	
Ë		P2 volume			Level volume 0.00 Foam volume 0.00	-
		P3 volume			Feed volume 0.00	
<u>k</u>		P4 volume				
					Y scale BACK	
ф	;00 11;10 11;20			1	User:Admin	
- Powe	r supply alarm			_	11:04:44 A011	?

Figure 16.4. Trend visibility settings

H.	t°C:0.0 pH:-	Option	Y Scale		0	¢
	06/22/2022 12:35			1	Days ago	
8		Y Scale			$\Theta$ $\bullet$ $\bullet$	
		🚖 Temperature		- C	Temp.,°C 0.0	
		☆ pH			pH 0.00 Base volume 0.00	
		☆ P5 volume			0.00	
Ë		☆ P1 volume			Level volume 0.00	-
		☆ P2 volume			Feed volume 0.00	
<u>~~</u>		☆ P3 volume				
		☆ P4 volume			Y scale	
					BACK	
\$	00 11 10 11 20				User:Admin	-
Power	supply alarm				15 11:04:44 A011-	?

Figure 16.5. Trend Y axis visibility settings

Additionally, the on-line graphical view of the main process parameters are displayed within the REACTOR window (highlighted in Figure 17.6).

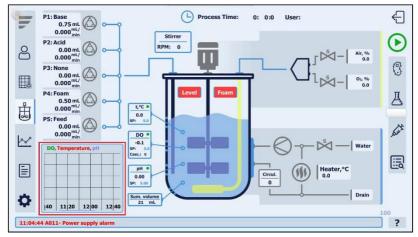


Figure 16.6. Trend section within the REACTOR window

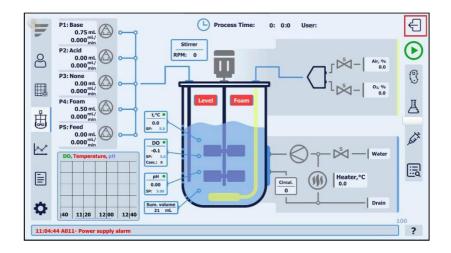
## 17. ALARM SIGNAL SETTINGS

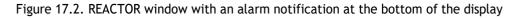
To access the alarm off set settings use the following access path MENU  $\rightarrow$  SETTINGS (1<sup>st</sup> WINDOW)  $\rightarrow$  ALARM OFFSET FROM SETPOINT, see Figure 17.1

T	t°C:0.0 pH:0.00	DO:-0.1	Casc. 0	) Process	: Time: 0: 0 :0	¢
0	Limits		Setpoints		Deadzone	
8	Stirrer min	100 RPM	Temperature	36.0	°C	
	Stirrer max	800 RPM	pH	7.00	+/- 0.20	
	O2 enrichment max	30.0 %	DO	50.0	%-sat +/- <u>5.0</u> %-sat	
	Feed rate min	50.0 %	Filling time	30	Sec	
	Feed rate max	0.0 %	Foam pump period	10	Sec	
O			Foam pulse length	3	Sec	
₿			Level pump off delay	10	Sec	
00	Alarm offset from set	point	Initial volume	2000	_mL	)
			P1 pump productivity	5.000	_mL/min	
200	DO +/-	5.0	P2 pump productivity	5.000	_mL/min	
	pH +/-	0.20 0.1 °C	P3 pump productivity	5.000	mL/min	
	Temperature +/-	0.1°C	P4 pump productivity	5.000	mL/min	
Ē						
E	C					
*						
~			• • •		User: Admin	
						109
		11:04:4	4 A011- Power supply a	larm		?

Figure 17.1. ALARM OFFSET window

The alarm offset window allows setting-up Low and High alarm limits for temperature, pH and  $pO_2$ . An alarm is triggered as soon as the process value drops below or goes over the pre-set limit - the alarm notification appears in red text in the bottom of the display, e.g. see Figure 17.2.





The information about the time of the event, cause of the event and date is displayed in the alarm notification.

If the reason for the alarm is resolved (e.g. during regulation the parameter already is within the required limits or the operator has switched off the alarm signal), the text disappears.

List of alarm notifications (Figure 17.3) can be found by using the access path MENU  $\rightarrow$  ADMINISTRATION  $\rightarrow$  ALARM.

μ	t°C:0.0 pH:0.00	DO: -0,1 Casc. 0 - Process Time: 0: 0: 0 - English
ප	Login	Alarms Events Date Time ACK time Message
	New user Delete user	06/22/2022 11:04:44 11:04:51 A011- Power supply alarm
₿	Change password	
<u>k~</u>		
Ē		
Φ	Disable alarms	User:
		11:04:44 A011- Power supply alarm ?

Figure 17.3. ALARM notification window

By using the access path MENU  $\rightarrow$  ADMINISTRATION  $\rightarrow$  DISABLE ALARMS, it is possible to open the list of alarms, where it is possible to mark the alarms, for which upon triggering a notification will be displayed in the bioprocess controller, see Figure 17.4.

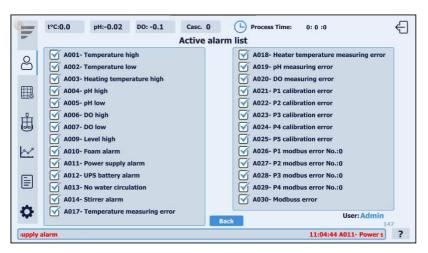


Figure 17.4. Active alarm list window

#### 17.2 SYSTEM EVENTS

List of event notifications (see Figure 18.5) can be found by using the access path MENU  $\rightarrow$  ADMINISTRATION  $\rightarrow$  EVENTS. In the EVENTS window the user can gain access to a database, which displays a list of all actions, which were performed with the system in a chronological order. Additionally, information on the previously active user, event type, equipment state etc. is provided within the mentioned window.



Figure 17.5. EVENT HISTORY window

## **18. PID PARAMETERS OF PROCESS CONTROL**

Bioprocess controller is applied to ensure precise regulation of process parameters. Their control software work according to the proportional-integral-derivative (PID) algorithms.

Such algorithms determine the extent of processes control signal effect on the performing mechanism. The regulation signal magnitude is calculated with the following equation:

$$u(t) = Pe(t) + l \int_0^t e(\tau) d\tau + D \frac{de(t)}{dt}$$

where,

- u(t) extent of effect in time t;
- e(t) error, i.e. difference between the set-point (SP) and the process value (PV);
- *P,I,D* proportional, integral and derivative ratio, respectively.

The proportional P ratio determines the effect directly proportional to e(t). The larger is P, the more sensitive is the effect. If P is too large, the regulation may de-stabilize due to intensified oscillations. If P is too small, the regulated parameter reaches the set-point value (SP) too slowly or may fail to reach it at all. Using only the proportional P ratio, in most cases sufficient preciseness of regulation cannot be achieved.

The integral ratio I determines the effect considering the mean summary error in the specific time. As a result, regulation becomes more stable and advanced. The set-point value (SP) of the regulated parameter is being reached faster.

The derivative ratio D determines the effect of the control signal considering the speed of change of the regulated parameter. For example, if the temperature set-point during the regulation process SP = 37 °C and PV = 35 °C, the algorithm determined the magnitude of the control signals output. The respective control elements implement the regulation, the temperature reaches the set-point value in a specific amount of time. If the situation will be similar, but the amount of time needed for the parameter to reach the set-point value will differ, the D parameter comes into place and corrects the output control signals magnitude. The P and I ratios do not consider the dynamics of value changes, and therefore correct setting of the D parameter is of utmost importance for dynamic processes to ensure sufficient preciseness of regulation.

In addition to the aforementioned ratios the following parameters can be set in the PID parameter window:

*Period* - determines the time delay after which the changes of regulating effect take place. Such parameter is working with considering sensor and process momentum.

*Time lag* - time lag of the derivative action. The algorithm of the D action includes a time lag that can be assigned at the "time lag of the derivative action" input.

# 18. PID PARAMETERS OF PROCESS CONTROL

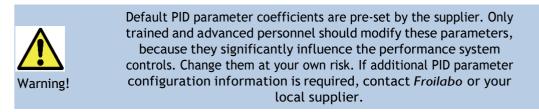
### 18.1 SETTING UP PID PARAMETERS

Open the PID settings window by using the access path MENU  $\rightarrow$  SETTINGS (3<sup>rd</sup> Window) highlighted in Figure 18.1.

	Heating temperature	DO st	irrer		DO enrich	ment	DO feed
S ≣	Prop. gain82.40Integr. time313.6Deriv. time79.7	Prop. g Integr Deriv.	time	0.03 0.0 0.0	Prop. gain Integr. time Deriv. time Fine	0.01 0.0 1.7 tuning	Prop. gain Integr. time Deriv. time Fine tuning
ᡱ <	Cooling temperature           Prop. gain         20.00           Integr. time         313.6           Deriv. time         79.7	06/22	/2022 10	:31:44			Sampling 20 Sec. Pause sampling Stirrer: 0 RPM DO PV: 0.0
Ē							DO SP: 0.0 02: 0.0 % Feed: 0.000 ml/min
ð		19:00	09;20	09:40	10;00 10;	20 10;40	Save all parameters User: Admin

Figure 18.1. SETTINGS window (PID)

PID parameter coefficients for heating, cooling,  $pO_2$  stirrer,  $pO_2$  feed,  $pO_2O_2$  enrich., pH base, and pH Acid can be modified in the PID configuration window.



The BioReactor system provides options for fine-tuning the PID control algorithms in respect to the peculiarities of different cultivation/fermentation processes. The user can enable auto tuning of PID coefficients during a running fermentation for the following process parameters: DO control by stirrer, DO control by  $O_2$  enrichment and DO control by feeding.

In order to enable the auto tuning procedure press the Fine tuning button in the respective PID coefficient section and then press the Start tuning button (see Figure 18.2). After enabling fine tuning the user can terminate the procedure at any time by pressing the Stop tuning button. If the procedure is terminated prior reaching the end-state, the new PID coefficients will not be saved to the system. The auto tuning procedure is finished automatically., to access other PID parameters press buttons PID 1, PID 2 and PID 3 to navigate through the PID configuration window.

# **18. PID PARAMETERS OF PROCESS CONTROL**



Figure 18.2. Window for auto tuning of DO control PID parameters

### **19. FEED CONTROL**

The Bioreactor system ensures feeding control by two options: by (1) feeding control with time profile and (2)  $pO_2$  concentration control.

#### 19.1 TIME PROFILE OF FEEDING RATE

In the bioreactor system the possibility to control feeding by means of adjustable profile has been envisioned. The following passage describes the principles of working with the profile.

	No.	Time, min	F, ml/min	No.	Time, min	F, ml/min		Feeding functions
9	1	0	5.000	11	5	5.000		Start
	2	5	5.000	12	5	5.000		The table data is up to date. Save changes Cancel changes
₿	3	5	5.000	13	5	5.000		Clear table
∄	4	5	5.000	14	5	5.000	(+)	Clear Lable
-	5	5	5.000	15	5	5.000		Feed rate
~	6	5	5.000	16	5	5.000	4 Min.	0.000 ml/min
	7	5	5.000	17	5	5.000		Feeding time
	8	5	5.000	18	5	5.000	$\cup$	0: 0 :0 HH:MM:SS
	9	5	5.000	19	5	5.000		
\$	10	5	5.000	20	5	5.000		User: Admin

The feeding profile window can be opened using the following access path: MENU  $\rightarrow$  FEED.

Figure 19.1. FEED window, TIME SHIFT pop-up window

Within the FEED window (Figure 19.1) it is possible to set-up 20 values of time and corresponding feeding rates. Time tags correspond to the fermentation process time.

During the process it is possible to adjust the feeding profile. Corrections will be taken into account on actual (running) feeding profile points, beginning of the next minute.

In the FEED window it is also possible to move the whole feeding profile either further or backwards in respect to the process time by using the Time Shift function.

Using time shift it is possible to change the time of the feeding profile time by subtracting or adding the necessary time (in minutes) to all feeding profile points. To do so, enter the desirable time and use buttons "-" to subtract or "+" to add the entered time to the profile points, see Figure 19.1.

Feeding is activated by pressing the START FEED button. Feeding rate will be activated depending on the defined process times and selected feeding profiles approximation. Feeding can be stopped using the same button that indicates STOP FEED while the feeding profile is active. When zero values

are introduced into the feeding profile time, the feeding will be terminated despite if further in the profile different values are entered.

## **19. FEED CONTROL**

### 19.2 DISSOLVED OXYGEN (DO) CONTROL BY FEEDING RATE

Dissolved oxygen control is maintained at a pre-set level, by automatically adjusting the feeding (substrate addition) rate.

If the SP (Set Point) and DZ (Dead Zone) for the  $pO_2$  value are defined, the stirrer operates in such a way, to maintain the process  $pO_2$  value at: SP  $\pm$  DZ. If the processes  $pO_2$  value (PV) is inside the dead zone corridor SP  $\pm$  DZ, the PID output value is calculated, but feeding rate adjustments are not implemented (no action is taken). Feeding is carried out as defined by the feeding profile. The feeding rate control can be carried out only if the feeding is in progress. If the processes  $pO_2$  value (PV) is outside the dead zone corridor SP  $\pm$  DZ, then the feeding rate is adjusted by the PID algorithm so that the PV returns into the dead zone corridor, the following algorithm is implemented based on the sign of the proportional  $pO_2$  feed PID coefficient:

Feeding rate is decreased, if the PV < SP  $\pm$  DZ. The minimum pumps' productivity is limited by the S<sub>lim</sub> parameter (%). The S<sub>lim</sub> parameter is defined by the user (highlighted in Figure 19.2).

Feeding rate is increased, if the PV > SP  $\pm$  DZ. The maximum pumps' productivity is limited by the S<sub>max</sub> parameter (ml/min). The S<sub>max</sub> parameter is defined by the feeding profile.



Figure 19.2. Feed profile parameters:  $S_{Max}$  and  $S_{lim}$ 

# 20. STARTING THE PROCESS

Before enabling the process, always carry out the activities listed below and inspect the respective system elements:

- 1) Check the operational conditions of the control system's software, bioreactor's tank, its constituents and other equipment;
- Make sure that the bioreactor tank is located correctly in respect to the bioprocess controller and respective service connections (more detailed explanations in Section 3.1: "INSTALLATION OF THE BIOREACTOR VESSEL");
- Make sure that all service connections have been carried out according to Section 3.4: "SERVICE CONNECTIONS";
- Carry out the calibration of sensors and pumps which are to be used during the process (information about calibration of each device is provided in the upper Sections of this user manual, see the table of contents);
- Make sure that the ports and their connections have been placed, screwed, connected, etc. correctly (more detailed instructions for the respective activities can be found in Section 3.2: "DESCRIPTION OF THE REACTOR LID AND PORTS", Section 3.3: "SENSOR" and Section 3.5: "VESSEL CONNECTIONS";
- 6) Carry out manual (in manual mode) inspection of the work of every control element, which is intended to be used during the process. It is necessary to ensure flawless operation of the system; therefore, potential errors/inconsistencies should be detected and solved;
- 7) Carry out sterilization of the bioreactor tank and its inputs (which will be in contact with the reaction environment) as described in Section 26: "STERILIZATION OF THE VESSEL";
- 8) Repeat steps 1-3, 5 and 6 after the sterilization of the bioreactor vessel and its inputs! Make sure that the reactor's tank is liquid-free (if it was not sterilized with the reaction environment or other liquids), and that the sampling port is closed.



Inappropriate equipment preparation for work may lead to serious physical injury or equipment damages. To avoid the upward mentioned, following instructions in this user manual, are highly recommended.

### 20.1 ADDING THE REACTION ENVIRONMENT TO THE BIOREACTOR VESSEL

When all activities listed in Section 20: "STARTING THE PROCESS" have been carried out, the reaction environment can be supplied to the sterilized bioreactor vessel.

To supply the reaction environment to the vessel, follow the instructions described further:

- 1) Connect the previously prepared vessel with sterile reaction environment to one of the needle ports or the chemostat tube, installed on the upper lid of the bioreactor, via a sterile hose;
- By using the feeding pump (see Section 10: "PUMP CONTROL") carrying out manual addition of the reaction environment to the vessel;



All connections should be performed in sterile conditions (e.g. in the presence of flame, laminar flow cabinet, etc.).

3) After reaction environment has been supplied, stop the pump, remove the previously connected tube and close the bioreactor port with a previously prepared sterile cap/plug

After the fermentation medium has been introduced into the bioreactor the user can setup the initial medium volume setting by following the access path: MENU  $\rightarrow$  SETTINGS (1<sup>st</sup> WINDOW)  $\rightarrow$  SETPOINTS

Limits		Setpoints	De	eadzone	
Stirrer min	100 RPM	Temperature	36.0 °C		
Stirrer max	800 RPM	pH	7.00 +/-	0.20	
O2 enrichment max	30.0 %	DO	50.0 %-sat +/-	5.0 %-sat	
Feed rate min	50.0 %	Filling time	30 Sec		
Feed rate max	0.0 %	Foam pump period	10 Sec		
		Foam pulse length	3 Sec		
		Level pump off delay	10 Sec		
Alarm offset from se	etnoint	Initial volume	2000 mL		
		P1 pump productivity	5.000 mL/min		
DO +/-	5.0	P2 pump productivity	5.000 mL/min		
pH +/-	0.20	P3 pump productivity	5.000 mL/min		
Temperature +/-	<u>0.1</u> °C	P4 pump productivity	5.000 mL/min		
				User: Adi	nin

Figure 20.1. Initial medium volume setting

#### 20.2 CONTROLLER SETTINGS FOR STARTING THE PROCESS

When all activities listed in Section 20: "Starting the process" have been carried out, the reaction environment can be supplied to the sterilized bioreactor vessel. To supply the reaction environment to the vessel, follow the instructions described further:

- 1) Connect the previously prepared vessel with sterile reaction environment to one of the needle ports or the chemostat tube, installed on the upper lid of the bioreactor, via a sterile hose;
- 2) By using the feeding pump (see Section 11: "Pump control") carrying out manual addition of the reaction environment to the vessel;
- 3) After reaction environment has been supplied, stop the pump, remove the previously connected tube and close the bioreactor port with a previously prepared sterile cap/plug.

The bioreactor system is ready!

#### 20.3 INOCULATION

It is recommended to carry out inoculation, using one of the three methods described below: (1) inject the microorganism culture into the reaction environment prior supplying it to the bioreactor tank, (2) using a peristaltic pump transfer the inoculum to the vessel after supplying the reaction environment to the bioreactors tank or (3) inject it into the bioreactor through the septa port. In all cases the activities have to be carried out in line with the instructions described in Section 20.1: "ADDING THE REACTION ENVIRONMENT TO THE BIOREACTOR VESSEL".

# 20. STARTING THE PROCESS

To eliminate the processes lag phase and to avoid improper fermentation conditions, it is recommended to inoculate the culture into the reaction environment with a temperature, that is close to the seed material and/or the processes temperature. The temperature can be maintained by adding the reaction environment with a desirable temperature to the bioreactor, or by manual or automatic temperature control of environment inside the bioreactor (see Section 6.1: "BIOREACTOR TEMPERATURE CONTROL").



Regardless of the chosen inoculation method, culture inoculation in the temperature and pH conditions far from desirable set points can irreversibly harm the culture.

# 21.PROCESS CONTROL WITH IOS/ANDROID TABLETS AND SMARTPHONES

The option for remote (WiFi) monitoring and control of the fermentation process using *iOS* or *Android* tablets and smartphones has been provided. The connection to the bioprocess controller is established via built-in router into the controller.

The *iTeleport* application should be installed on your device to gain access to the upper mentioned functions. Upon configuring and connecting to the bioprocess controller, you will acquire a visually and functionally identical copy of the bioprocess controller's display in your *iTeleport* app.

# 22. SAMPLING AND HARVESTING

The method of culture sampling and harvesting can vary depending on user requirements and fermentation process specifics. The suggested sampling and harvesting procedures for the bioreactor system are described below.

Both sampling and harvesting actions can be performed through the lower port of the vessel - port (1) and port (2). For sampling it is common to use one of these ports and to close the other one with a specified needle port plug. To start sampling or harvesting, open the tap by screwing it clockwise (see Figure 22.1)

The sampling volume can vary depending on:

The analytical measurement requirements;
The amount of the culture or product in the vessel;
The duration of the fermentation process;
Etc.

Typical sample volumes for the bioreactor system are 1 - 20 mL.

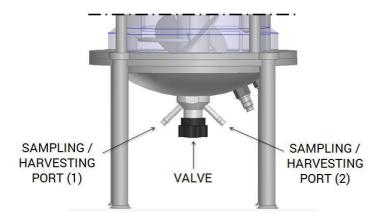


Figure 22.1. Sampling port

#### 22.1 SAMPLING AND SAMPLING CHANNEL STERILIZATION

In the bioreactor system an option to sterilize the sampling channel with steam is provided. Steam sterilized sampling line is shown in Figure 22.2.

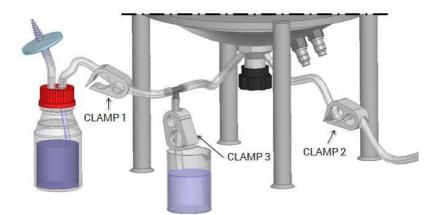


Figure 22.2. Sampling channel sterilization

In Figure 22.2 port (2) is used for the steam supply. The sterilization procedure is performed as follows:

- 1) Connect port (2) to the steam supply via temperature resistant silicone tube with an installed clamp (2);
- 2) Connect a short silicone tube to port (1). Connect the other end of the tube to a T-shaped divider;
- 3) Connect a short silicon hose with a clamp (3) to one end of the divider and place the end of the tube into a beaker filled with 70 % ethanol;
- 4) Connect a longer silicone hose with a clamp (1) to the second end of the divider and connect it to a small bottle filled with deionized water;
- 5) Sterilize the sampling channel by opening the clamps (1) and (2), and open the steam supply. Let the steam flow through the channel for about 1 2 min to sterilize the sampling line;
- 6) After sterilization has been carried out, close the clamps (1) and (2);
- 7) Take out the tube that is immersed in ethanol out of the beaker and put its end into the sample container. Open the bioreactor tap afterwards;
- 8) Open the clamp (3) and collect the necessary sample volume into the container, see Figure 22.3;

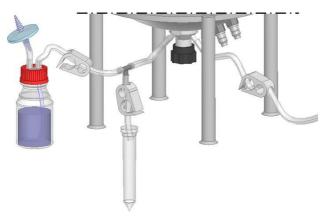
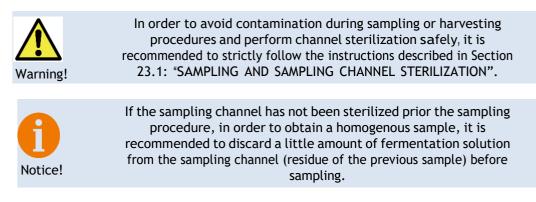


Figure 22.3. Sampling

- 9) After the sampling procedure has been carried out, close the clamp (3) and immerse the tube back into the beaker;
- 10) Close the tap.



After taking a sample the user can specify the subtracted volume of the medium to the in the REACTOR window (see Figure 22.4). The mentioned value upon entering will be taken into account during automatic logging of the medium volume.

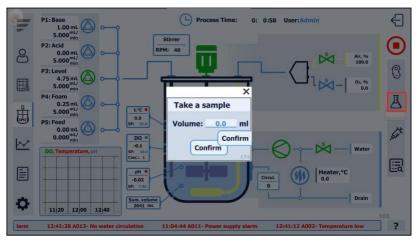


Figure 22.4. Sample volume window

#### 22.1 INDUCTION

Inductor agents and/or other substances can be added to the reaction medium via peristaltic pump or manually, by supplying the respective solution via septa port (*optional*) or through one of the free inlets located on the vessels upper lid. After adding an inductor to the medium the user can specify the added volume in the REACTOR window (see Figure 22.5). The mentioned value upon entering will be taken into account during automatic logging of the medium volume.

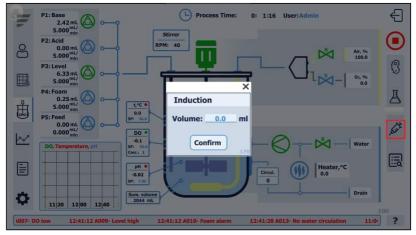


Figure 22.5. Inductor volume window

#### 22.2 HARVESTING

In order to perform sterile harvesting of the entire bioreactor environment at the end of the fermentation process, perform the activities described further:

- Prior harvesting, a sterile bottle or vessel should be prepared. Harvest bottle (large enough to hold the entire culture that is in the bioreactor vessel), should be equipped with a harvesting tube and a sterile filter for air exchange. The harvesting tube has to be long enough to reach from the bottle (placed lower than the vessel) to the lower part of the bioreactor's vessel where the sampling/harvesting port is located (see Figure 22.1);
- 2) When everything is prepared for the harvesting procedure, connect the harvesting tube to the sampling channel in aseptic conditions see Figure 22.2;
- 3) Open the bioreactor's tap (see Figure 22.1);
- 4) Open the clamp (3) (see Figure 22.2) and wait until the entire fermentation environment has been drained into the bottle;
- 5) Close the bioreactor tap and the clamp (3);
- 6) Aseptically disconnect harvesting tube from the sampling tube.

# 23. COMPLETION OF THE PROCESS

To stop the fermentation process, use the same access path as used when enabling the process: MENU  $\rightarrow$  REACTOR  $\rightarrow$  STOP.

For safety purposes, control elements (cooling valve, heater, stirrer, pumps, air valve and  $O_2$  valve) should be switched to Manual mode after the process has been stopped.



Turning the control elements to Manual mode after the process run, minimizes the risk of unplanned system operation and its damage upon accidental launch of process simulation!

# 24. CLEANING OF THE VESSEL

After the process has been stopped, disconnect the bioreactor vessel from all service communications.

Carefully remove sensors from the tank. Follow instructions listed in Section 27: "MAINTENANCE", to ensure appropriate maintenance and storage of the pH and pO<sub>2</sub> sensors.

Thoroughly wash and clean the bioreactor vessel and the corresponding parts (ports, sensors, etc.).

Unscrew the outlet air condenser according to the instructions outlined in Section 3.1: "INSTALLATION OF THE BIOREACTOR VESSEL".

Bioreactor turbine removal and cleaning is highly recommended after every fermentation process, see instructions on Section 3.2: "DESCRIPTION OF THE REACTOR LID AND PORTS".

# **25.STERILISATION OF THE VESSEL**

To sterilize the vessel in the autoclave, follow the instructions described below:

- 1) Install all necessary sensors and other accessories in the bioreactor's tank, taking into account that the bioreactor has to be hermetical during the sterilization procedure;
- 2) Fill the vessel with distilled water or culture media if high temperatures and pressure will not affect its chemical composition;



During vessel sterilization it is highly recommended to prevent the sensors from being dry through the procedure, therefore, fill the bioreactor with liquid in order to avoid any possible sensor damage.

3) Disconnect the motor and all sensor cables;



Never put any electrical cables into the autoclave for sterilization, this can cause irreversible damage!

4) Disconnect all silicone tubes from the reagent bottles. Close the tube ends by putting clamps on them - as close to the tube ends as possible;



Tubes have to be clamped in order to prevent any liquid efflux from the bioreactor vessel during sterilization.



During sterilization tubes can burst or slip off the inlet ports due to overpressure or damaged tubes. Therefore - sterilize only tubes that are intact, thoroughly rinsed -

never sterilize tubes if they are filled with corrective reagents!

- 5) Place the bioreactor vessel into the autoclave;
- 6) Carry out the vessel sterilization (120 °C for 45 min is recommended);
- 7) When the sterilization procedure has been finished and the vessel has cooled down, take it out of the autoclave and place it in its planned working location;
- 8) Carry out required operations, which are to be made with the bioreactor.

	In order to avoid severe skin burns due to the high temperature:
	<ul> <li>Always wear protective clothes and heat resistant gloves while working with the autoclave or any other hot equipment.</li> </ul>
<u> </u>	<ul> <li>Ensure that all devices are cooled down to room temperature before use.</li> </ul>
Warning!	- It is recommended to place a suitable warning notice e.g. "Hot".

### 26 MAINTENANCE

In the following sections the maintenance and preparation procedures for the  $pO_2$  and pH sensors are described. Keep in mind that the information in this user manual should be comprehended together with the information supplied by the sensor's manufacturer.

### 26.1 MAINTENANCE AND STORAGE OF THE PH SENSOR

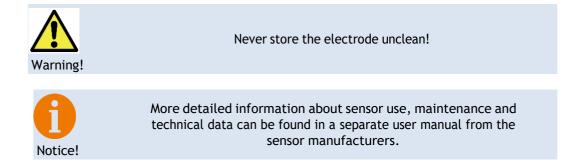
After receiving the sensor, carefully remove all packaging, cut off the protective rubber layer from the sensors upper membrane, if such is supplied. Wash the sensor with distilled water and wipe it dry it with a clean paper towel. Afterwards, the sensor should be fastened on a stand and immersed in a 0.3 M KCl solution for several hours.



Never let the pH sensor rest on its tip! Sensor's maintenance and storage should be done only while the sensor is fastened to a stand.

Inspect the lower part of the sensor for any gas bubbles. If any bubbles are present, eliminate them by shaking the sensor in a vertical motion. After the electrode is removed from its delivery package it should be stored on a stand and immersed in 0.3 M KCl solution, so that the upper membrane is submerged into the liquid.

If the sensor will not be used for a long period of time, it must be immersed in a 3 M KCl solution.



### 26.2 MAINTENANCE AND STORAGE OF THE PO<sub>2</sub> SENSOR

After working with the sensor, its surface must be cleaned and washed with distilled water.



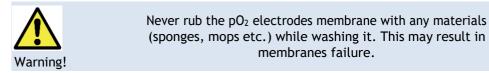
Never store the electrode unclean! Never let the  $pO_2$  sensor rest on its tip! Sensor maintenance and storage should be done while the sensor is fastened to a stand.

While the sensor is not being used the membrane chamber must be filled with the  $O_2$  electrolyte, and the electrode tip should be closed with the protective lid. Electrolyte must be changed every 3 months while storing the sensor. If the predicted period of storage will exceed 6 months, the sensor must be stored dry (i.e., without filling the membrane chamber with electrolyte). If the sensor is stored dry, we don't recommend connecting it to a power supply (i.e.,  $pO_2$  measuring device).

#### Sensor features

The sensors cable contact socket must be inspected prior to connection to make sure it is dry. Moisture, corrosion and dirt in the socket may result in false sensor measurements. Cable of the sensor also should be inspected, to ensure that there are no signs of insulation or socket damage.

Before commencing the calibration, visual inspection of the sensor membrane must be performed. If any dirt on the membranes surface is noticed it must be washed with distilled water.



If any signs of damage are found on the membrane it must be replaced. The membrane should be replaced in case if the sensor reading inertness increases.

Do not use solutions containing alcohol for sensor cleaning. This may result in permanent damage of the sensor.



More detailed information about sensor use, maintenance and technical data can be found in a separate user manual from the sensors' manufacturers.

#### 26.3 STIRRER MAGNETIC SHAFT MAINTENANCE

Periodic lubrication of the stirrer magnetic shaft bearings is recommended, to extend the shaft's lifetime. Magnetic shaft's maintenance after 1-2 years is recommended. Please, follow the instructions listed below (see Figure 26.1) to perform the upper mentioned procedure.

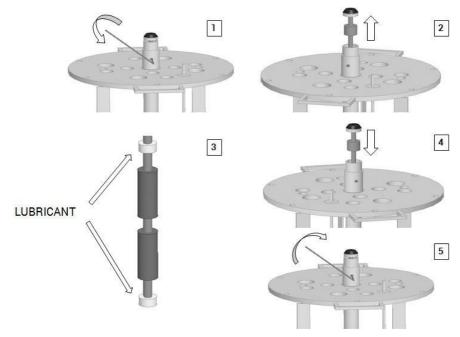


Figure 26.1. Illustrations of the magnetic shaft maintenance procedure

- 1) Using one 36 mm wrench, loosen the screw located on the upper part of the stirrer shaft;
- 2) Carefully pull out the inner magnetic shaft;
- Add the supplied grease on both shafts bearings. The amount of grease should be enough to cover the upper part of the bearing, we advise to put grease in an about 1 mm thick layer. The supplied grease is recommended for lubrication of metallic parts, which are subjected to diminish in high temperatures;
- 4) After adding the grease, carefully insert the inner magnetic shaft back into the outer agitator shaft. To maintain the appropriate magnet position, it is important insert magnetic shaft to its full extent;
- 5) Using the 36 mm wrench, firmly tighten the screw on the upper part of the stirrer shaft.

### 26.4 REACTOR VESSEL HERMETICITY TESTING

Periodic hermeticity test ensures that the vessel is completely hermetically sealed and ready for operation, Pressure leak could lead to vessel being infected by foreign microorganism. Most hermeticity leaks can be attributed to wear and tear, which can be addressed and corrected by using the supplied spare O-ring set and silicone sealant use for O-ring sealing. It is needed to perform the test on the vessel if there is a suspicion of an air leakage from the fermenter.

To test the hermeticity of the vessel all the ports on vessel should be plugged and hermetically sealed, lid should be tightly screwed on top and condenser exhaust port should be closed using the membrane valve. There should be no path for air to escape from the vessel.



Never exceed pressure of 1 bar when testing for hermeticity! Higher pressures could lead to glass tube cracking and exploding.

The test should be performed accordingly:

- 1) Make sure all paths for air to escape are closed with plugs or sensors Leave level and foam indicator in the vessel for hermeticity tests around the seals.
- 2) Attach air source to the air input port of the control cabinet (see Figure 3.9); make sure to adjust appropriate (not too high) air source pressure.
- 3) Set the pressure on manometer in front of the control cabinet in AIR section (see chapter 8, AIR/O<sub>2</sub> SUPPLY SETTINGS, Figure 8.1).
- 4) In control panel close O<sub>2</sub> supply valve and open AIR valve, open the rotameter fully and wait for rotameter to show that there is no air flow in the line and all the air is now compressed in the vessel.
- 5) Close air AIR valve in control panel and wait for 10 minutes without changing the line pressure or performing any other parameter changes.
- 6) While waiting notice if there are any obvious air leakage sounds in any part of the system or vessel, if any area is suspected, then a spray of water in the affected area would reveal leak if there is bubbling present.

- 7) After waiting 10 minutes open the air supply valve again and note if rotameter is indicating any air flow in the system. System is hermetically sealed if there is no extra air flow in the system after opening it after 10 minute test.
- If there is a leak it should be noted and leak should be addressed by replacing the offending part or replacing the seal.

## 27.Help

For user convenience a copy of the user manual, which describes all relevant procedures and principles of working with the BioReactor system is provided within the bioprocess controller. To access the mentioned manual press the Help button, which is displayed on each window of the system (see Figure 27.1).

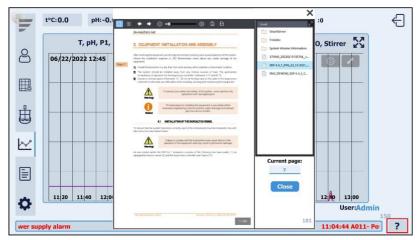


Figure 27.1. Help button